

ESTEP 2025 Annual Event

28-30 October 2025
Udine (ITALY)

How decarbonisation, digitisation
and circular solutions forge the
sustainable European steel future?

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MemKoWI & Sector coupling with Power4Steel:

New findings with pilot-scale CO_2 - and H_2 -separation by
membrane technology from industrial gases of steel-,
cement- and biomass-plants



Power4Steel supported by:

Ministerium für
Wirtschaft, Innovation,
Digitales und Energie
SAARLAND



Federal Ministry
for Economic Affairs
and Energy

MemKoWI supported by:

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Federal Ministry
for Economic Affairs
and Energy



DIGIMET



DANIELI AUTOMATION



**UNIVERSITÀ
DEGLI STUDI
DI UDINE**
HIC SUNT FUTURA

Conventional ore-based steel production route at DILLINGER:

Efficient steel production with internal gas reuse and high internal recycling-rates

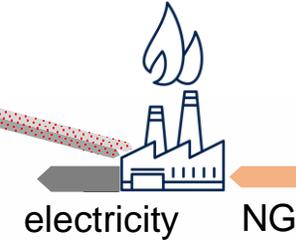
Power4
Steel



H₂-containing COG & H₂ + CO₂-containing BFG

to internal gas network

internal gas re-use



Where is CO₂ - and H₂ -separation desirable for enrichment & depletion?

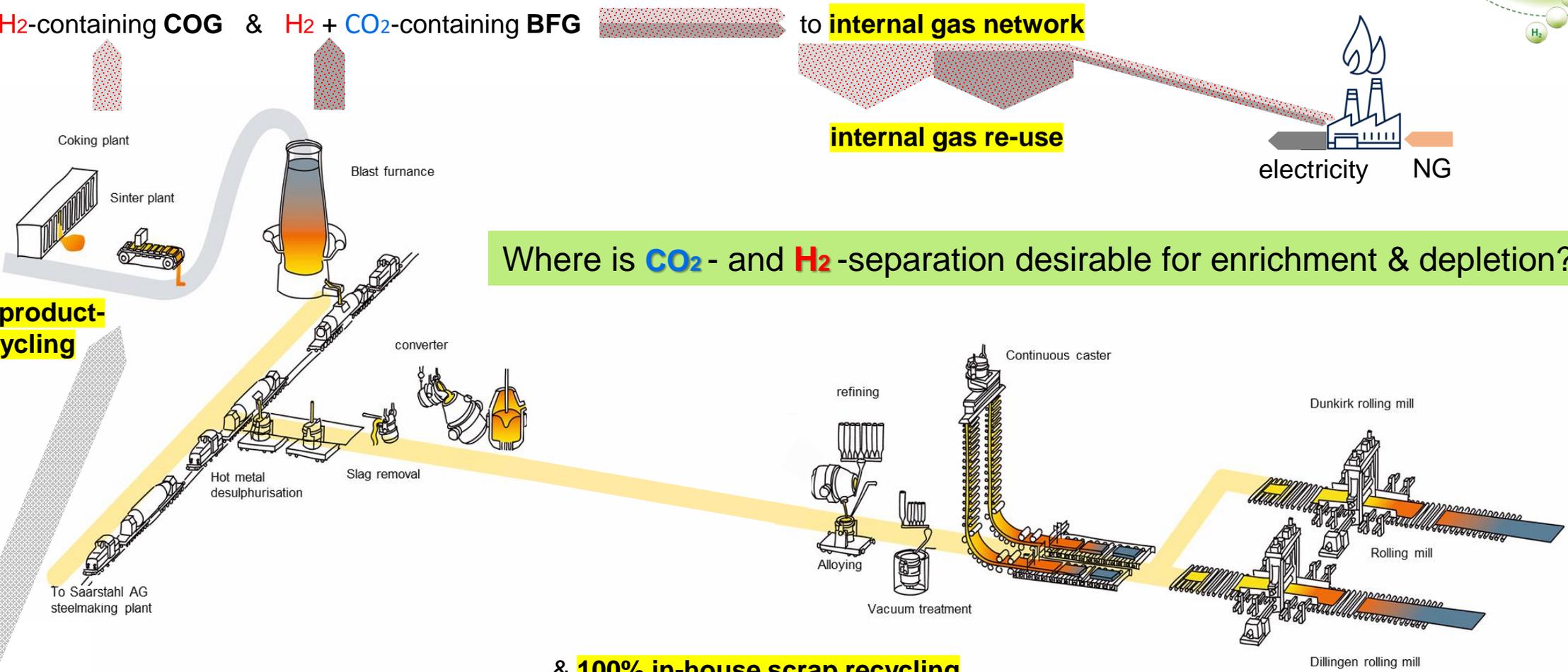
~95% by-product-recycling

& 100% in-house scrap recycling

internal pre-treatment of Fe-by-products (dust, sludge, scale, iron in slag)

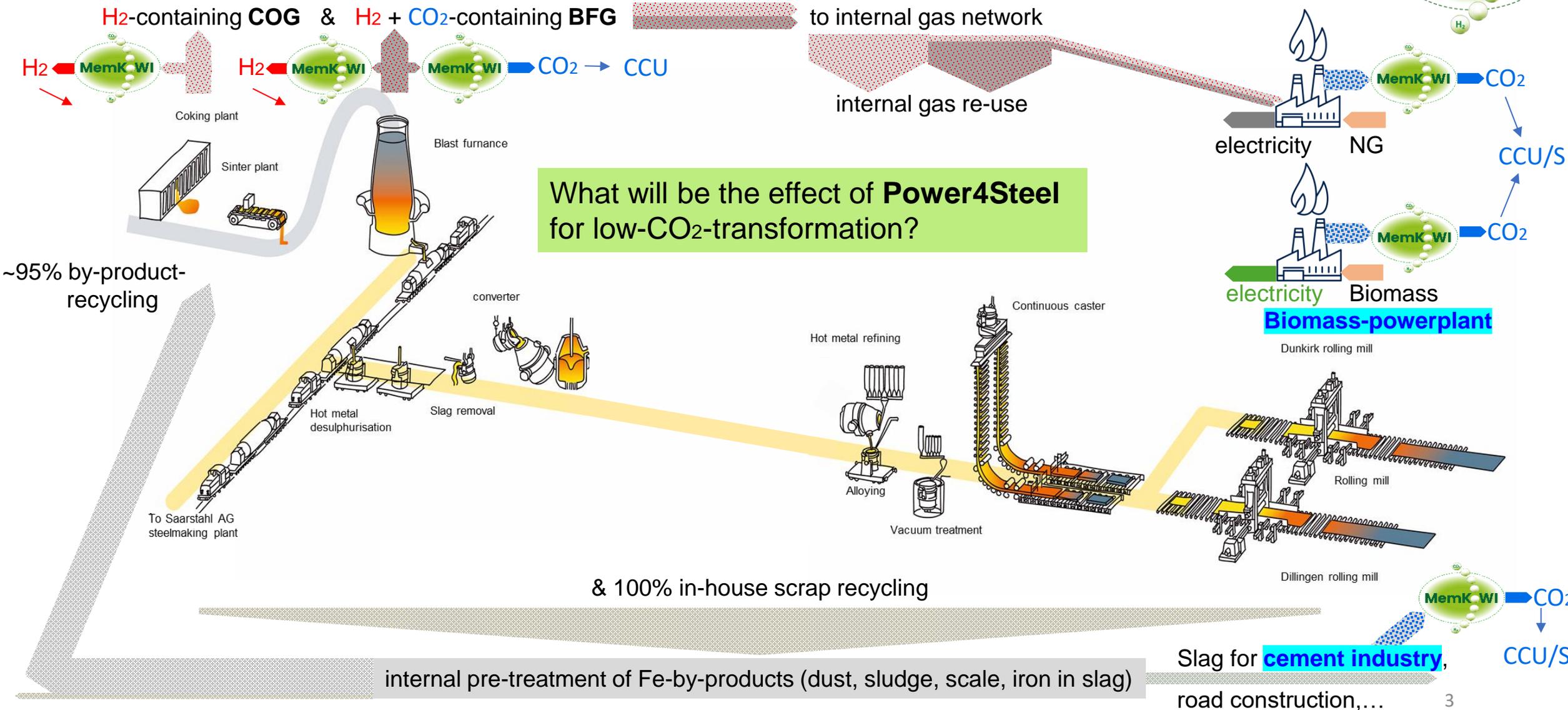
Slag for cement industry,
road construction,...

~5% landfill from by-products



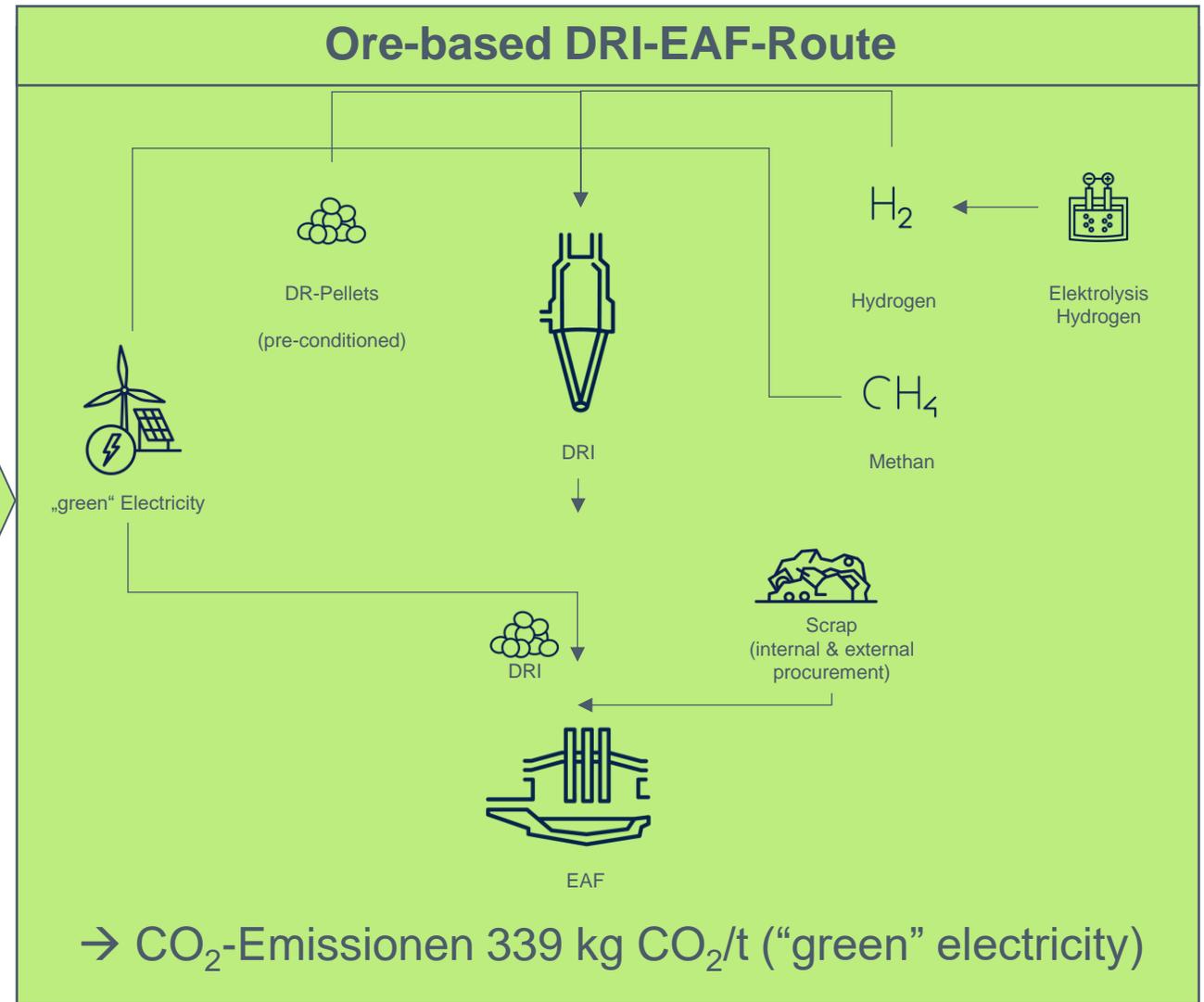
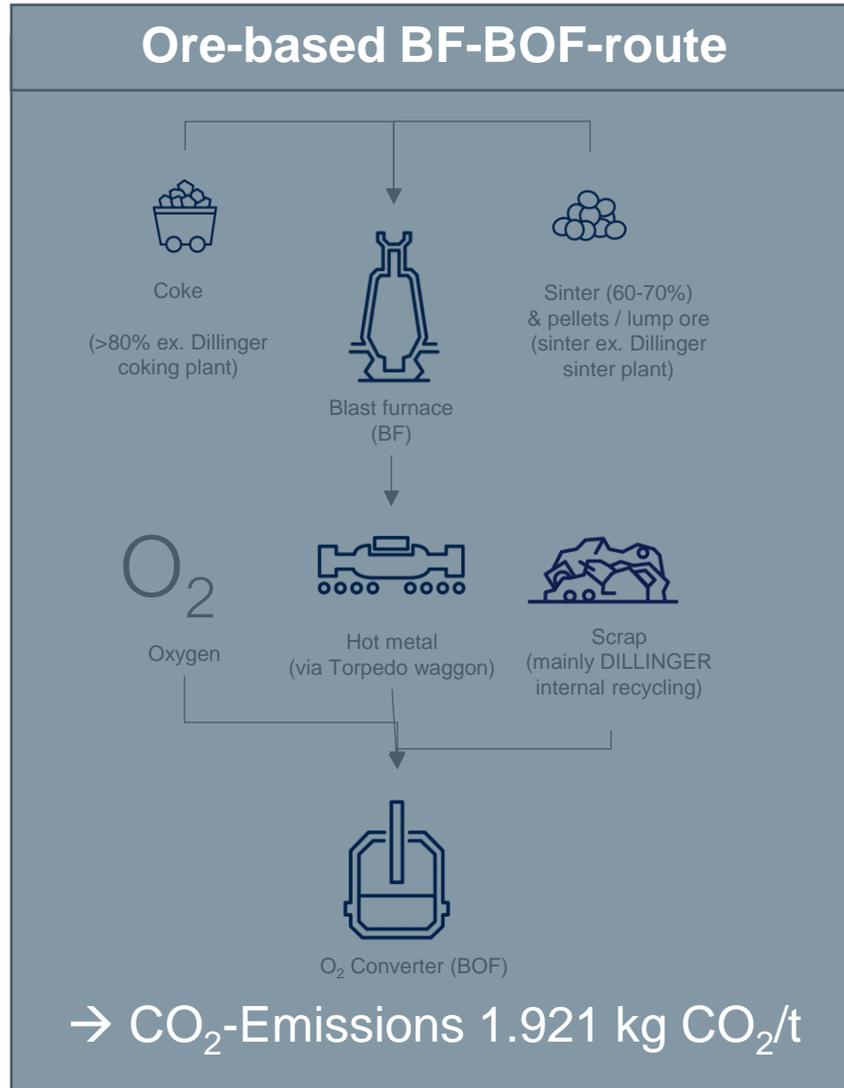
Conventional steel production route at DILLINGER with MemKoWI:

Optimization for reuse of H₂ and CO₂-containing gases including sector coupling



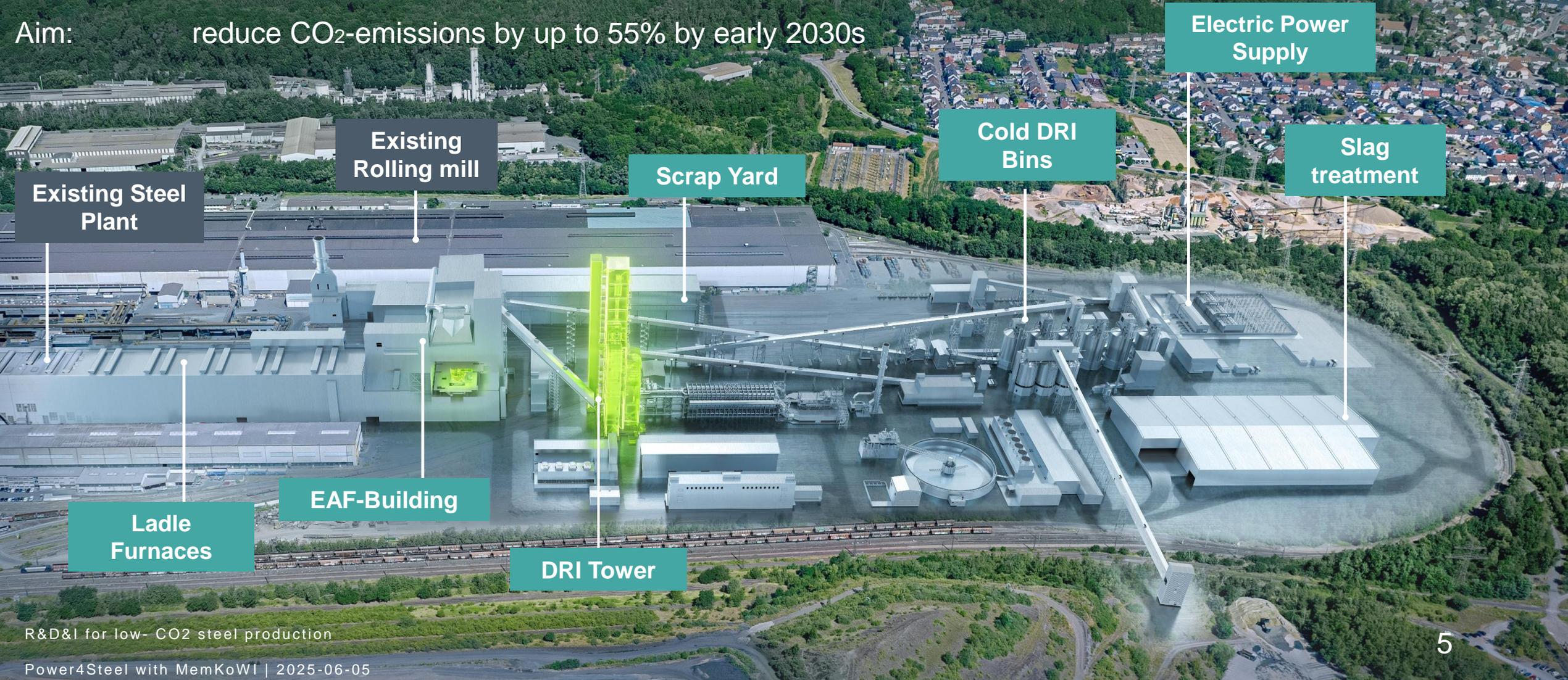
What will be the effect of Power4Steel for low-CO₂-transformation?

Steel production from „conventional“ to „green“ (= low CO₂)



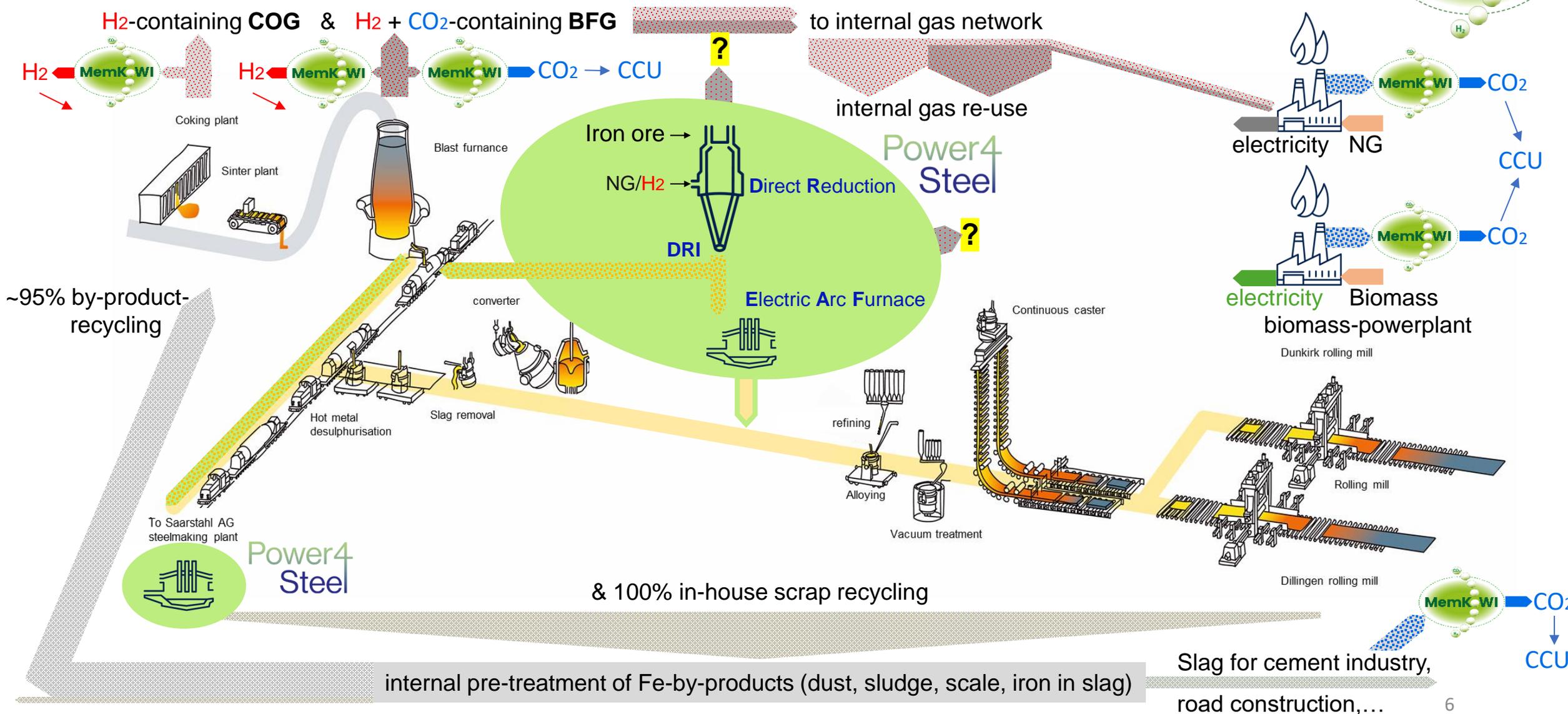
Power4Steel project – site at DILLINGER – construction is in progress:

Cost: €4.6 billion
Concrete: 300,000 m³
Steel used: > 100,000 t
Aim: reduce CO₂-emissions by up to 55% by early 2030s



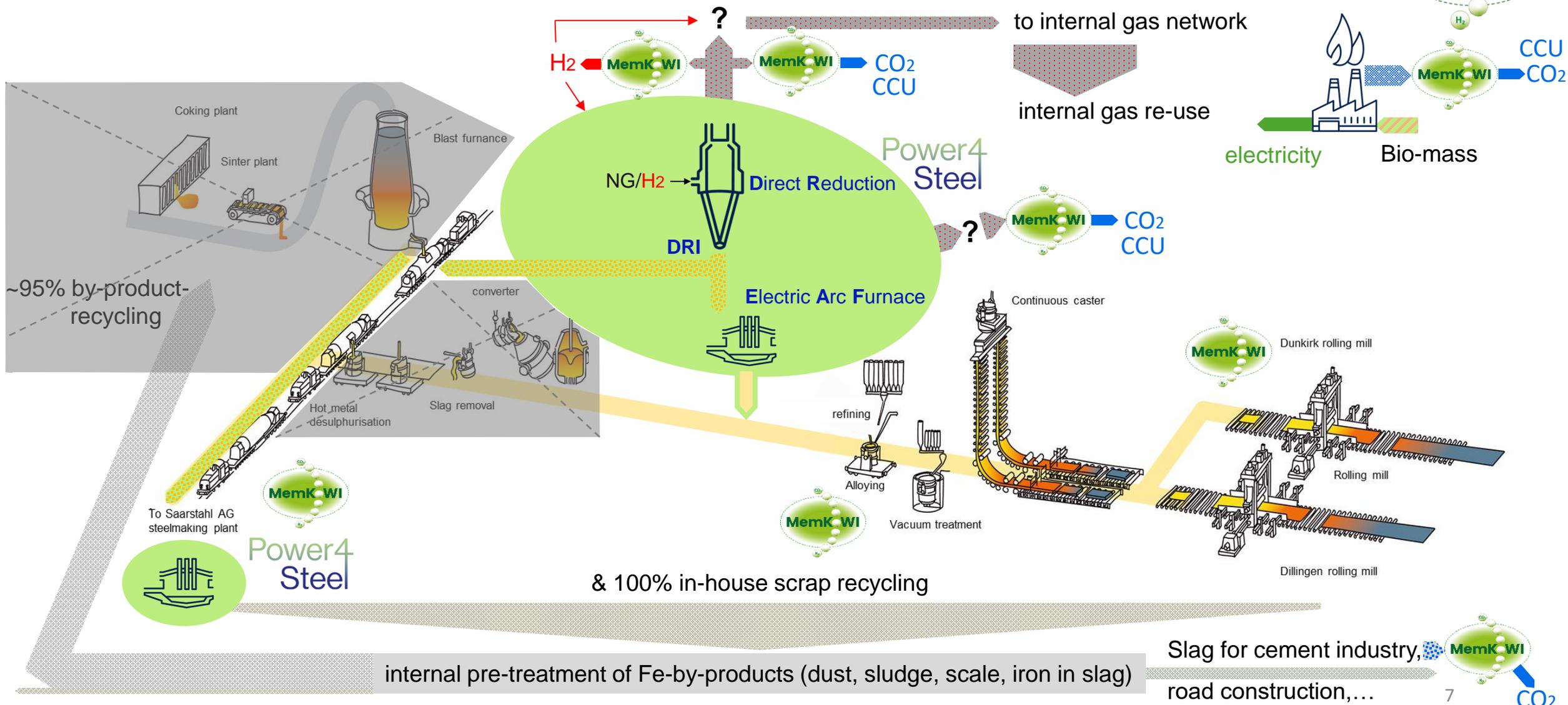
Power4Steel for ore-based steel production route at DILLINGER:

New gas compositions require further technology development for H₂ and CO₂



Power4Steel final step with MemKoWI-potential:

New challenges and technology gaps will emerge → further R&D&I is essential

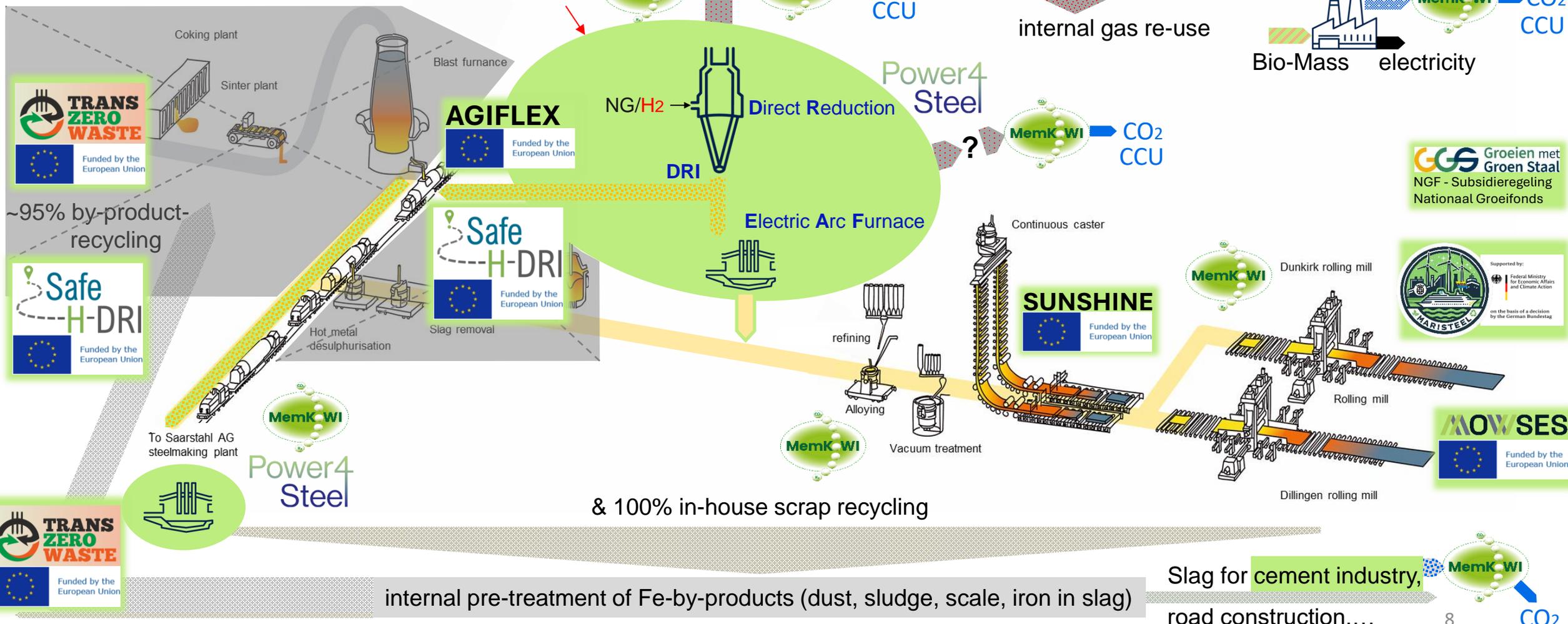


Power4Steel final step with R&D&I-projects support:

Power4Steel with synergetic R&D&I finds solutions to challenges and technology gaps!



Here are some examples:



~5% landfill from by-products

internal pre-treatment of Fe-by-products (dust, sludge, scale, iron in slag)

Slag for cement industry, road construction,...

The MemKoWI consortium – cross sectorial experts



<p>Research</p> <p>Membranes/Polymer Steel industry</p>  <p>Helmholtz-Zentrum hereon</p>  <p>Bfi Angewandte Spitzenforschung</p> <p>Membranes/Ceramic Gas technologies</p>  <p>JÜLICH Forschungszentrum</p>  	<p>Steel industry</p> 	<p>Cement industry / Plant design</p> <p>thyssenkrupp Polysius</p>
<p>Membrane production</p> 	<p>Regenerative energies</p> 	<p>Engineering</p> 

The project MemKoWI – cross sectorial challenges & targets



- **Testing & optimizing gas separation membrane technology**
 - Steel, CO₂ and H₂
 - Cement , CO₂
 - Biomass power plant, CO₂

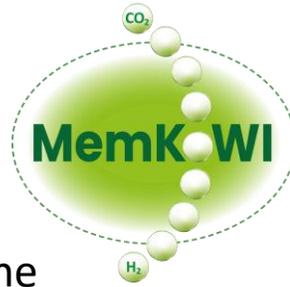
- **Optimized membranes and membrane modules**
 - Polymers
 - Ceramics

- **Digitalisation and modelling**

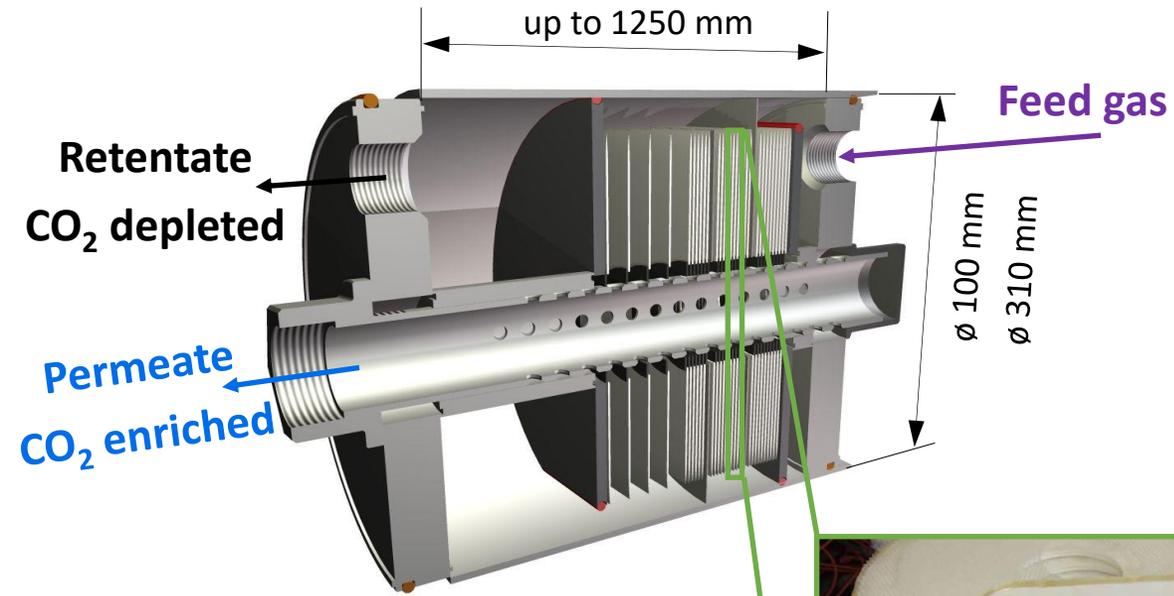
- **Expected outcome**
 - Up-scaling of membrane-technology for separation of CO₂ und H₂
 - Move TRL: 3-5 → 6/7 with concept for TRL 9
 - Provide an important element for sector coupling



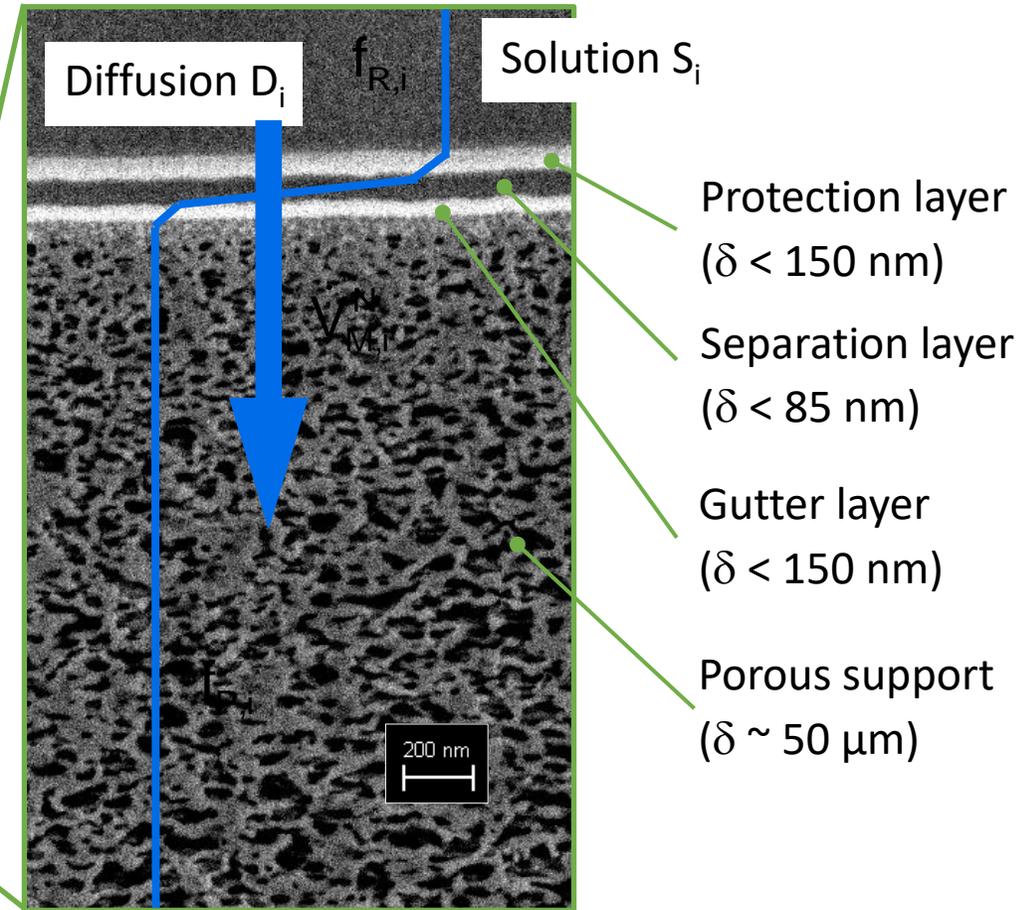
Membrane module and membrane – polymeric membranes



Envelope type membrane module



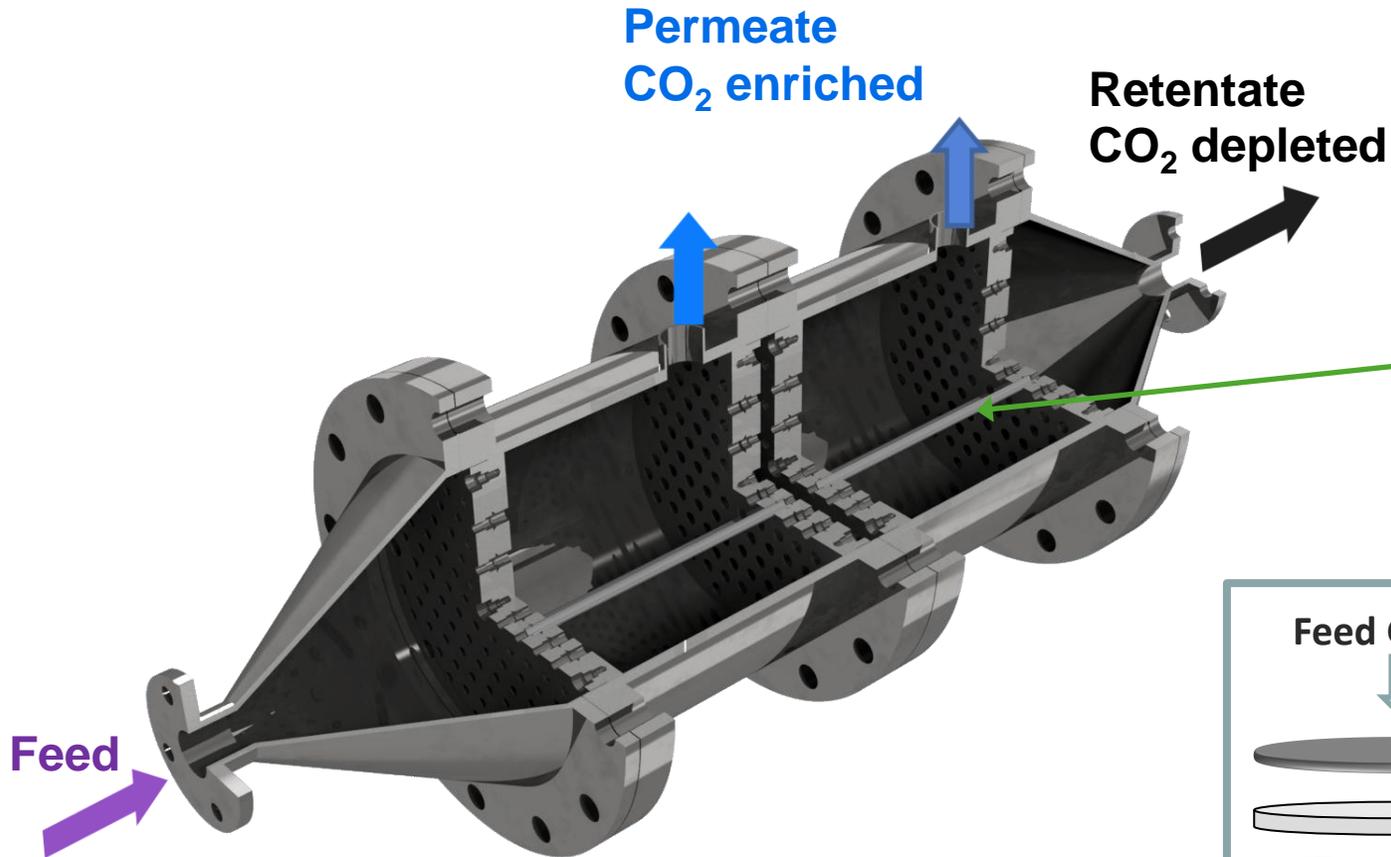
Cross section of thin film composite membrane



Membrane envelopes

- Rubbery polymers: selective for CO_2
- Glassy polymers: selective for H_2

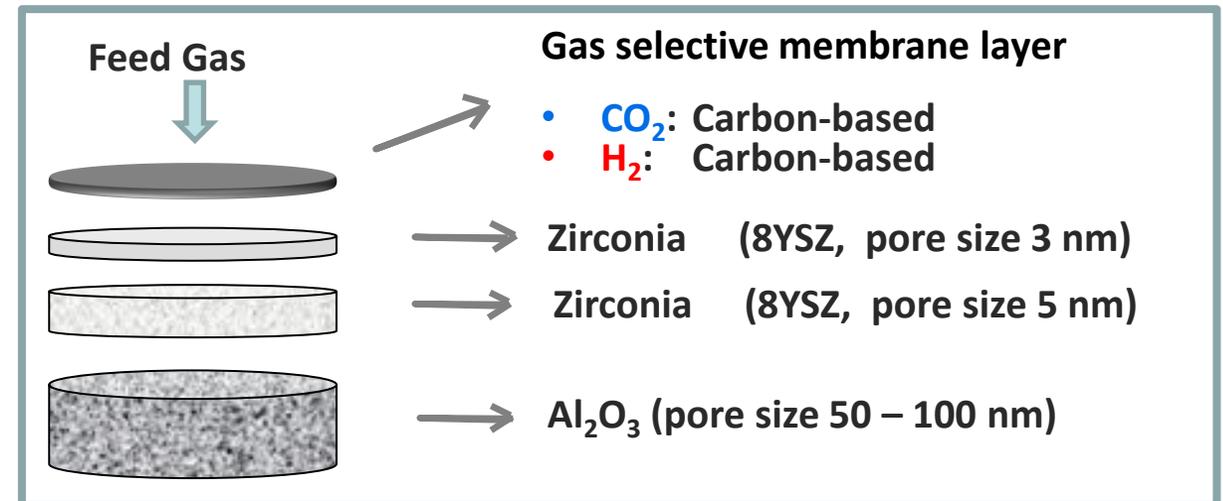
Membrane module and ceramic membrane



Ceramic membrane basis
 Al_2O_3 -tubes



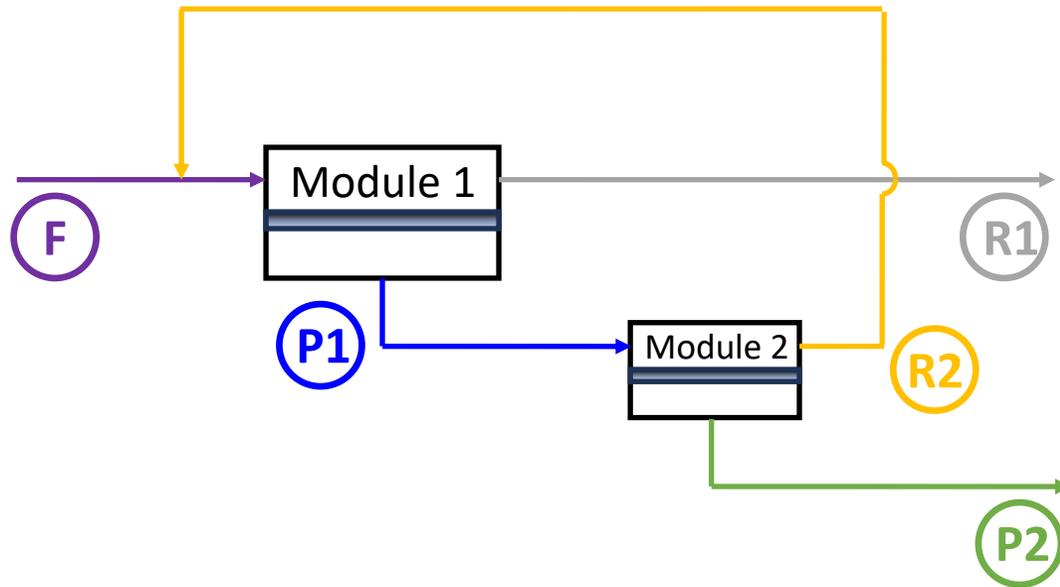
- $< 1 \text{ nm}$: **Surface diffusion** via adsorption and desorption, selective for CO_2
- $< 0.5 \text{ nm}$: **Molecular sieving**, selective for H_2



CO₂ separation from gas power plant flue gases (COG/BFG/NG)

Two stage mode – Polymer membrane

- Two stage process



Module 1 – polymer membrane:

- CO₂ selective PolyActive™
- Area A_M=16 m²
- Selectivity $\alpha_{CO_2/N_2}(\vartheta=25^\circ C) = 47$
- Permeance L_{CO₂} ($\vartheta=25^\circ C$) = 3 Nm³/(m² h bar)

Module 2 – polymer membrane:

- CO₂ selective PolyActive™
- A_M=0.74 m²
- $\alpha_{CO_2/N_2}(\vartheta=25^\circ C) = 47$
- L_{CO₂} ($\vartheta=25^\circ C$) = 3 Nm³/(m² h bar)

Module 2

Permeate 2:
CO₂

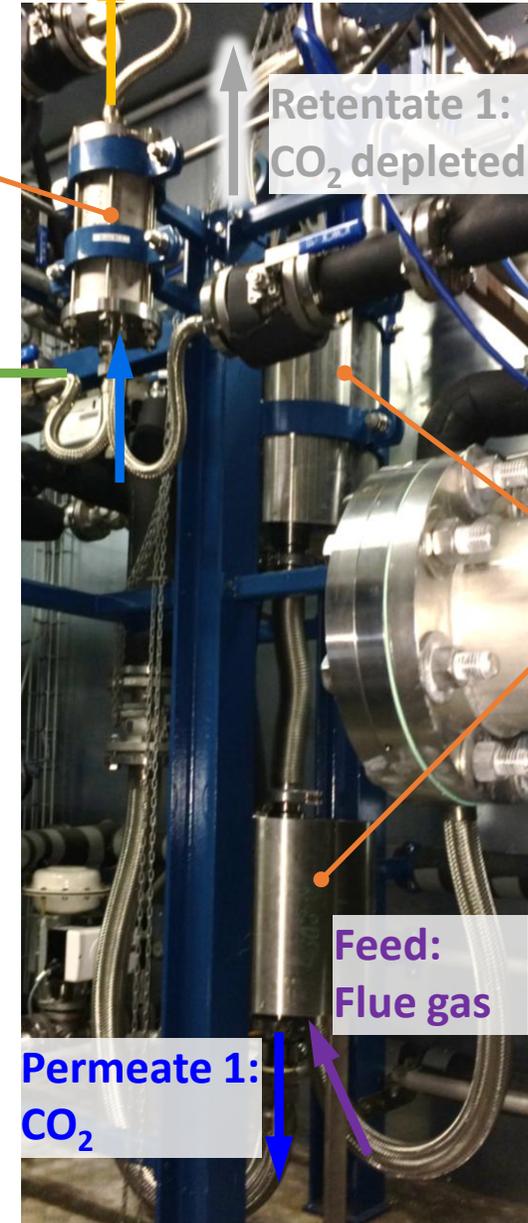
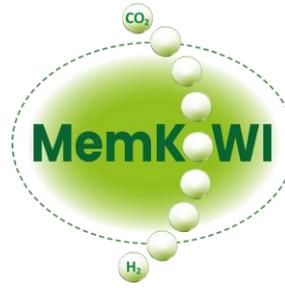
Retentate 2:
Recycled to Feed

Retentate 1:
CO₂ depleted

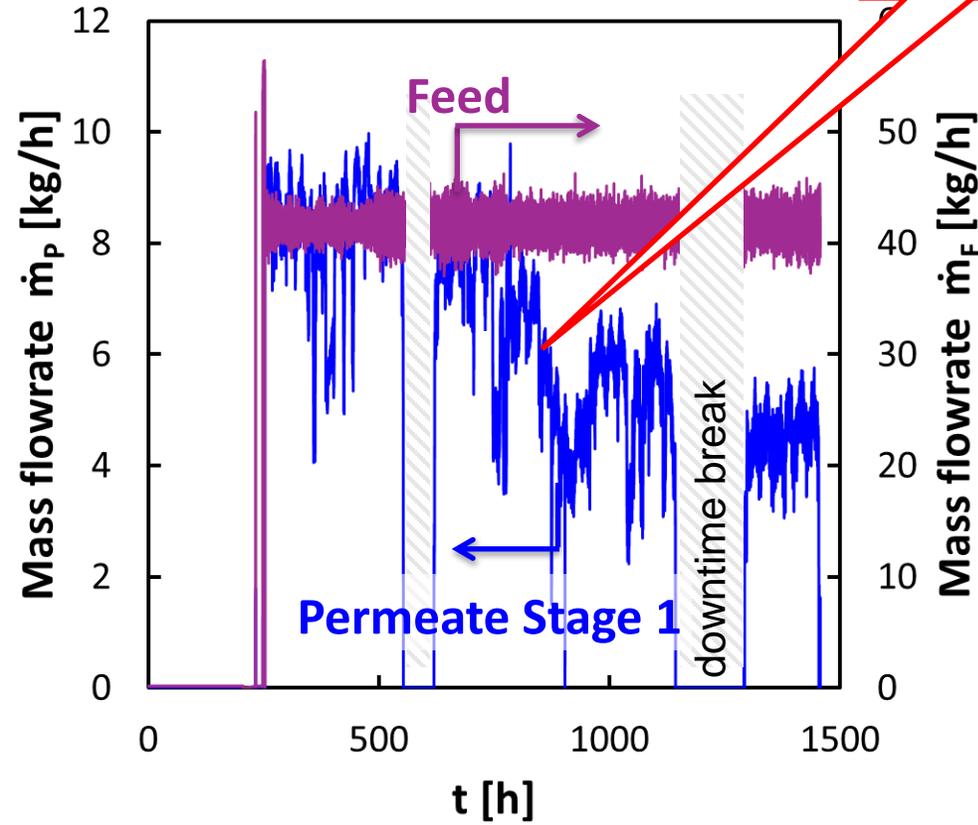
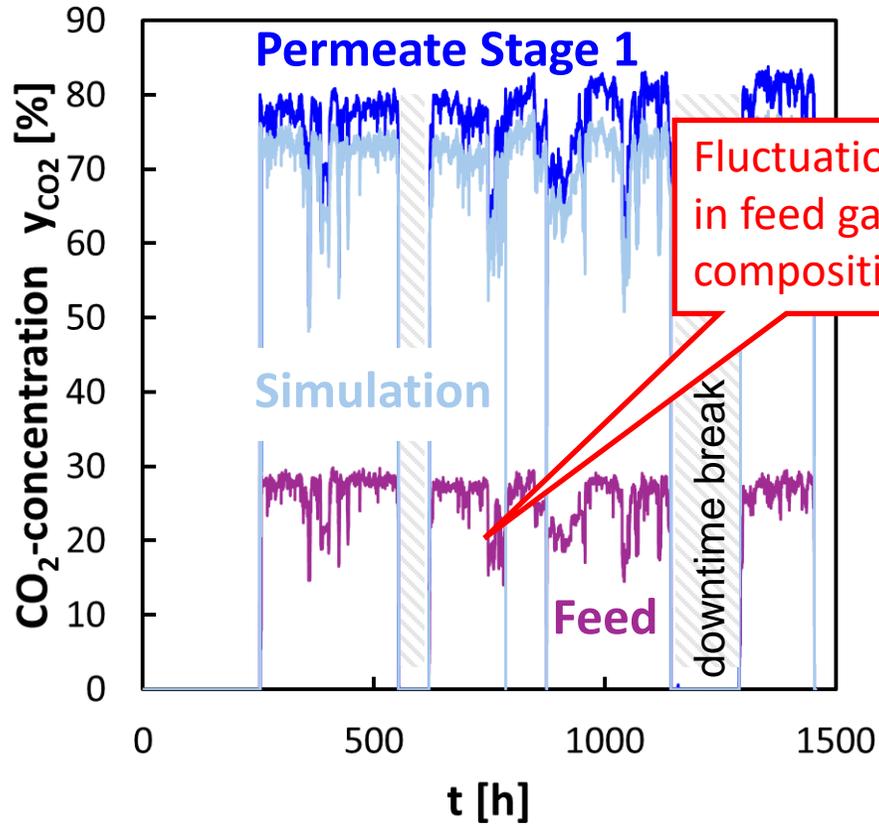
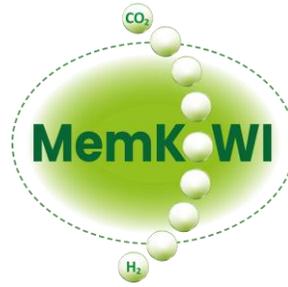
Module 1

Feed:
Flue gas

Permeate 1:
CO₂



Operating performance one stage mode – Polymer membrane

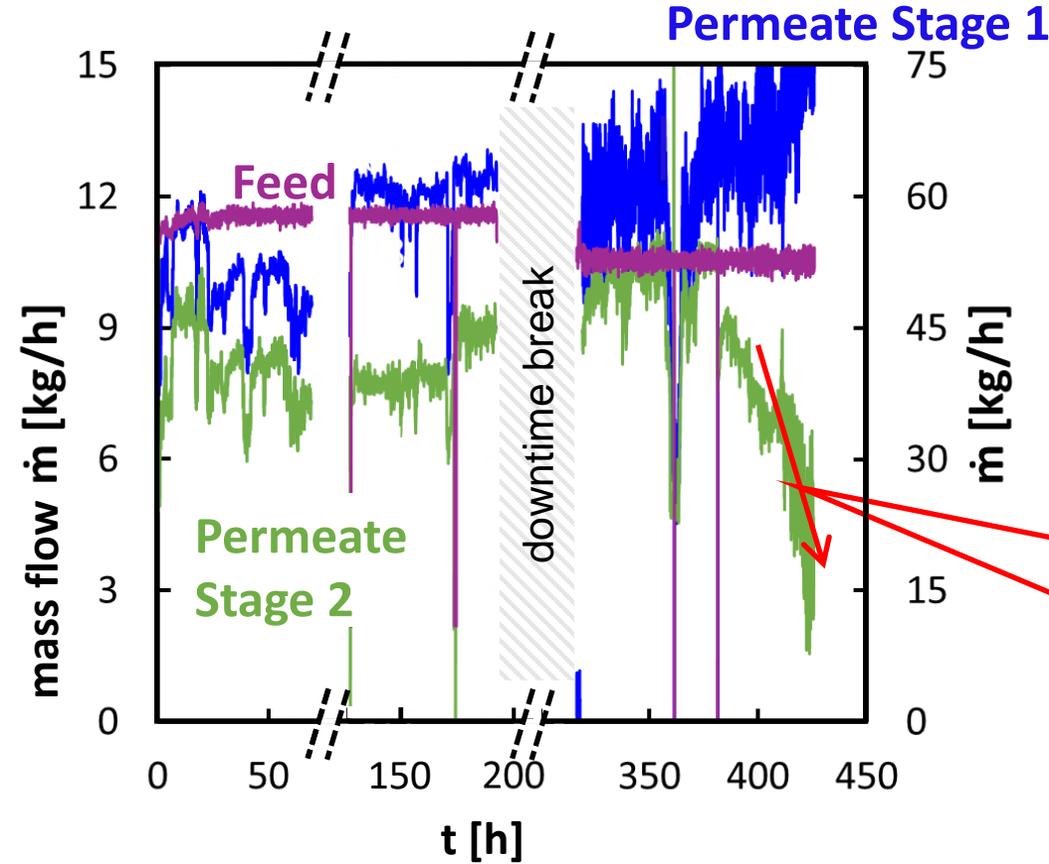
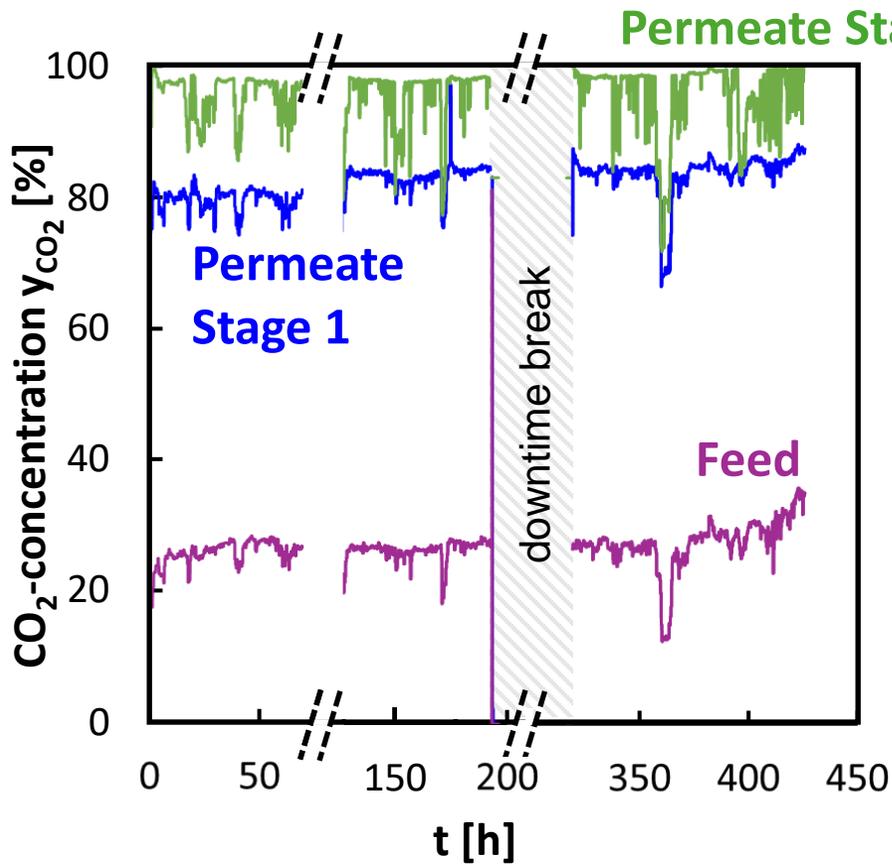
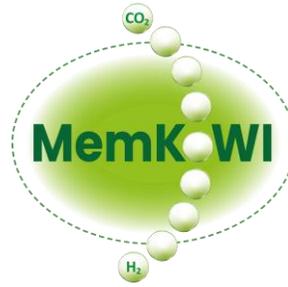


Observations:

- stable, two stage operation: **CO₂ in 1st stage permeate > 80 mol-%** ✓
- **no loss of performance** by downtime break ✓
- fluctuations in feed gas composition → drop in membrane performance

Use for up-scaling: - automated feed-gas related downtime control & gas dehumidification

Operating performance two stage mode – Polymer membrane



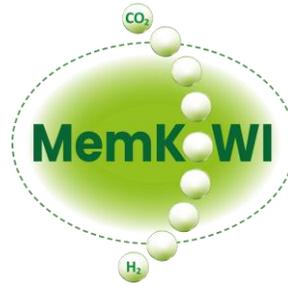
Water entrainment into module stage 2

Observations:

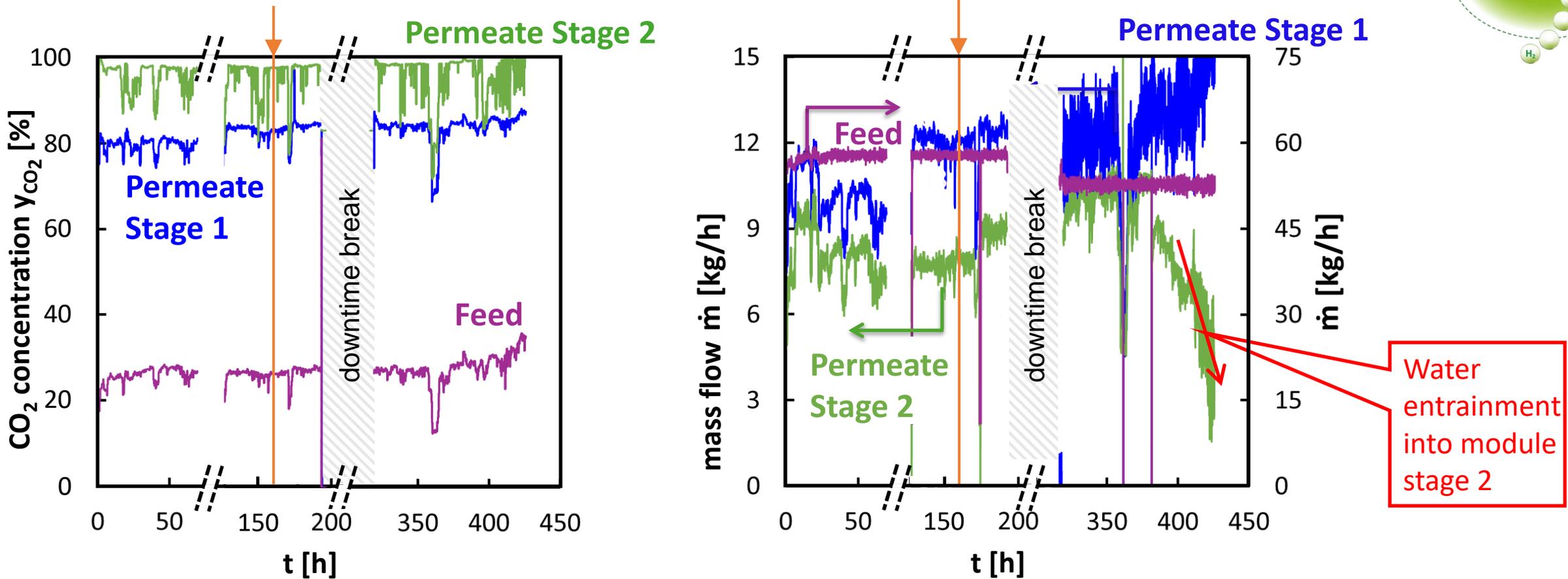
- stable, two stage operation: **CO₂ in 2nd stage permeate > 95 mol-% → fit for use ✓**
- **no loss of performance** by downtime break ✓
- water entrainment severely impacts performance → risk mitigation action at feed-side

Use for up-scaling: - automated feed-gas related downtime control & gas dehumidification

Operating performance two stage mode – Polymer membrane



Example after 160h operation

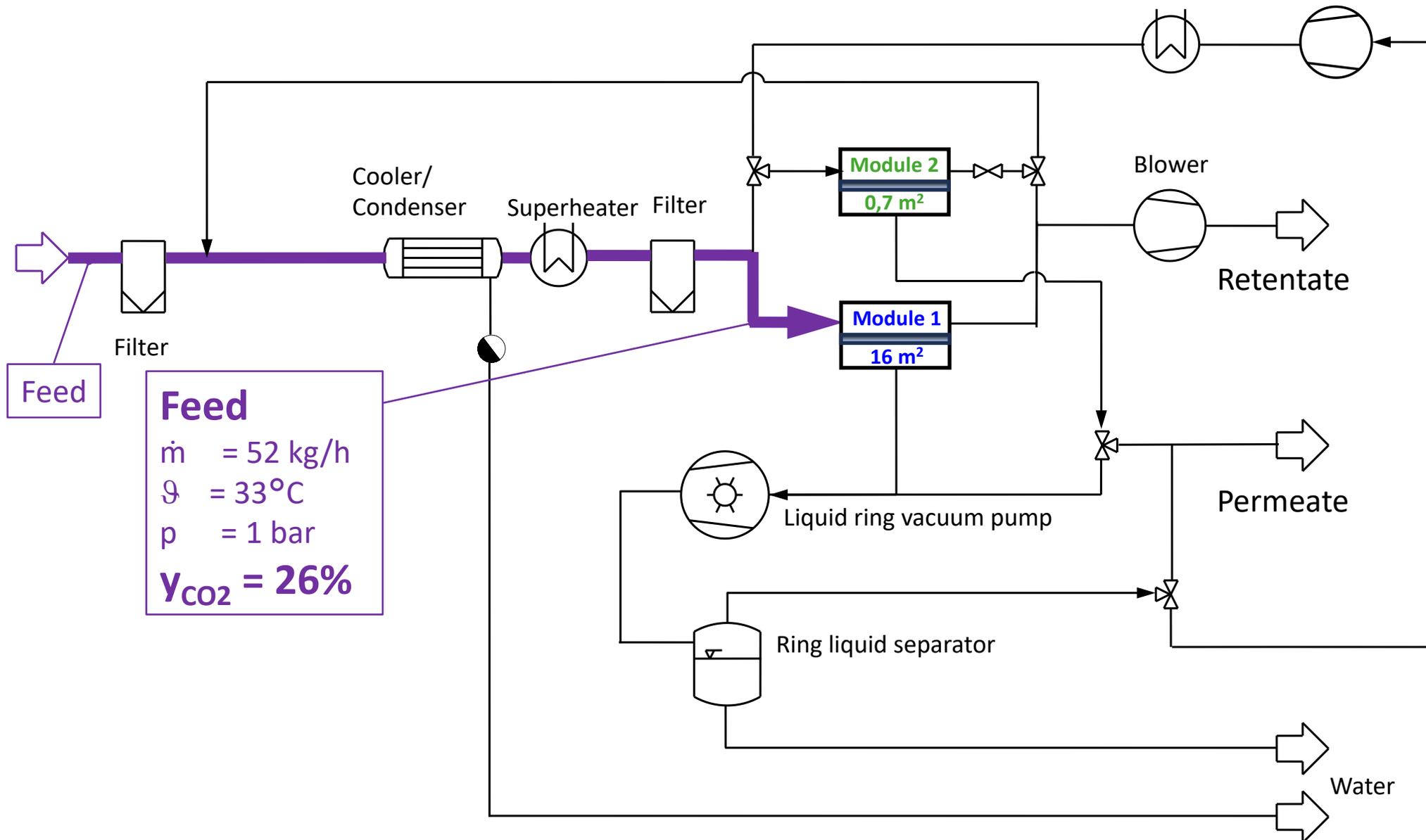
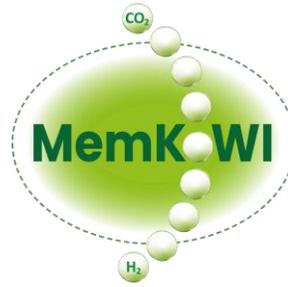


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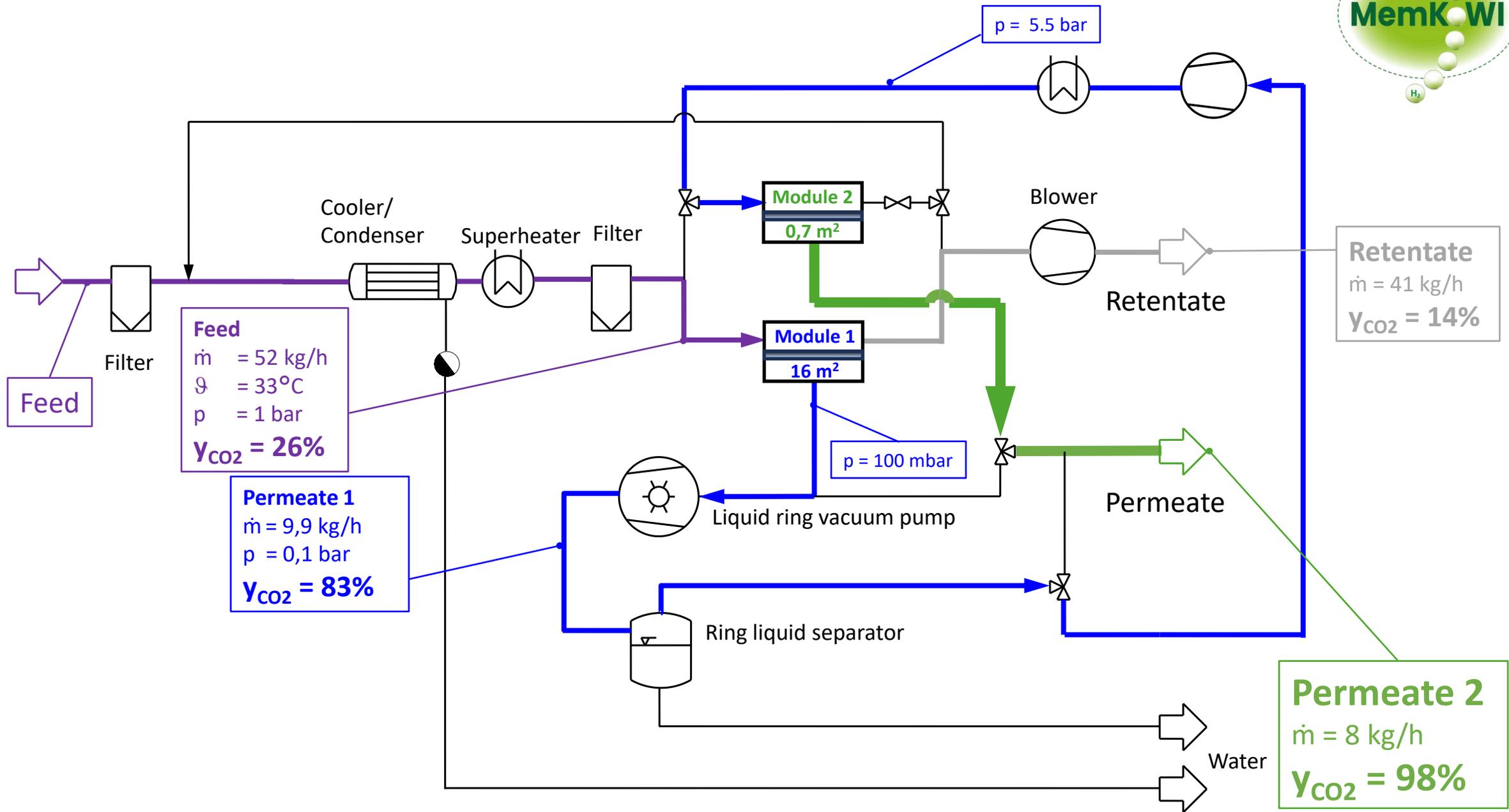
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Use for up-scaling: - automated feed-gas related downtime control & gas dehumidification

Example - Operating point after 160h (2-stage polymer membrane)



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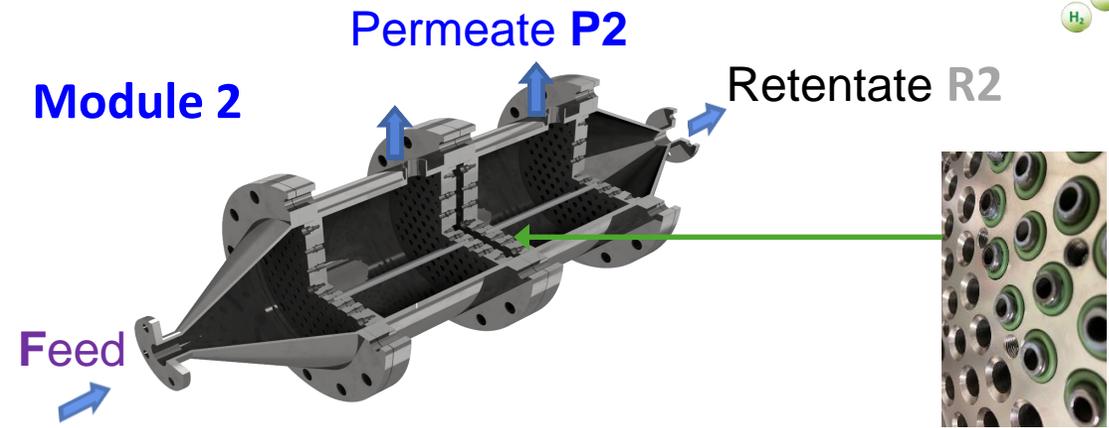
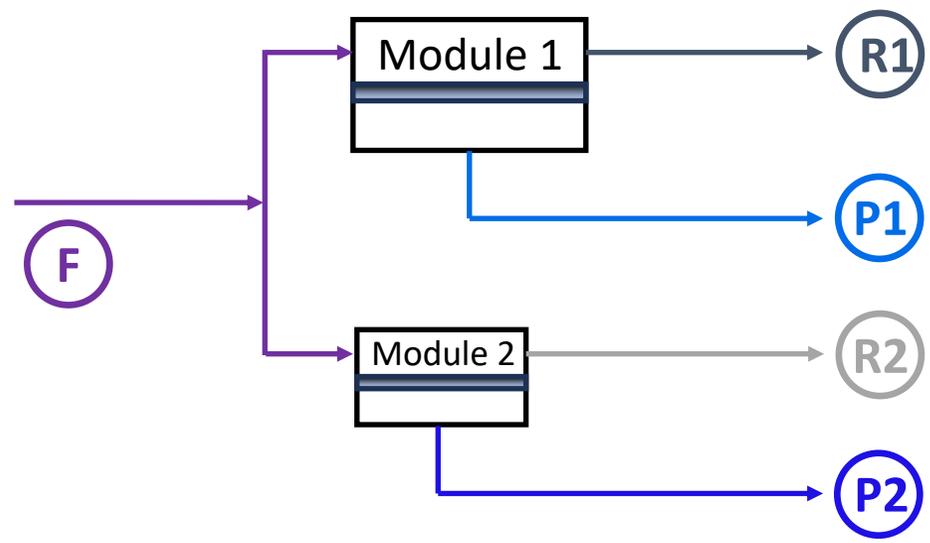


CO₂ separation from gas power plant flue gases (COG/BFG/NG)

One stage mode – for Ceramic and Polymer membrane



- Parallel operation



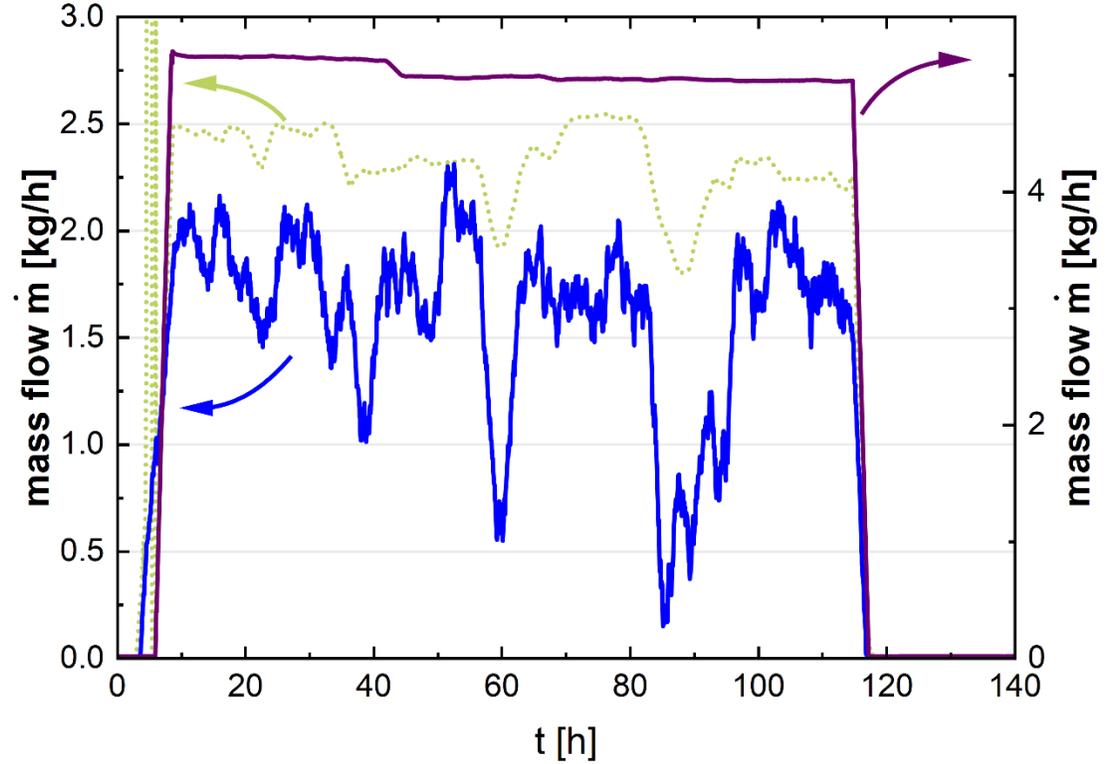
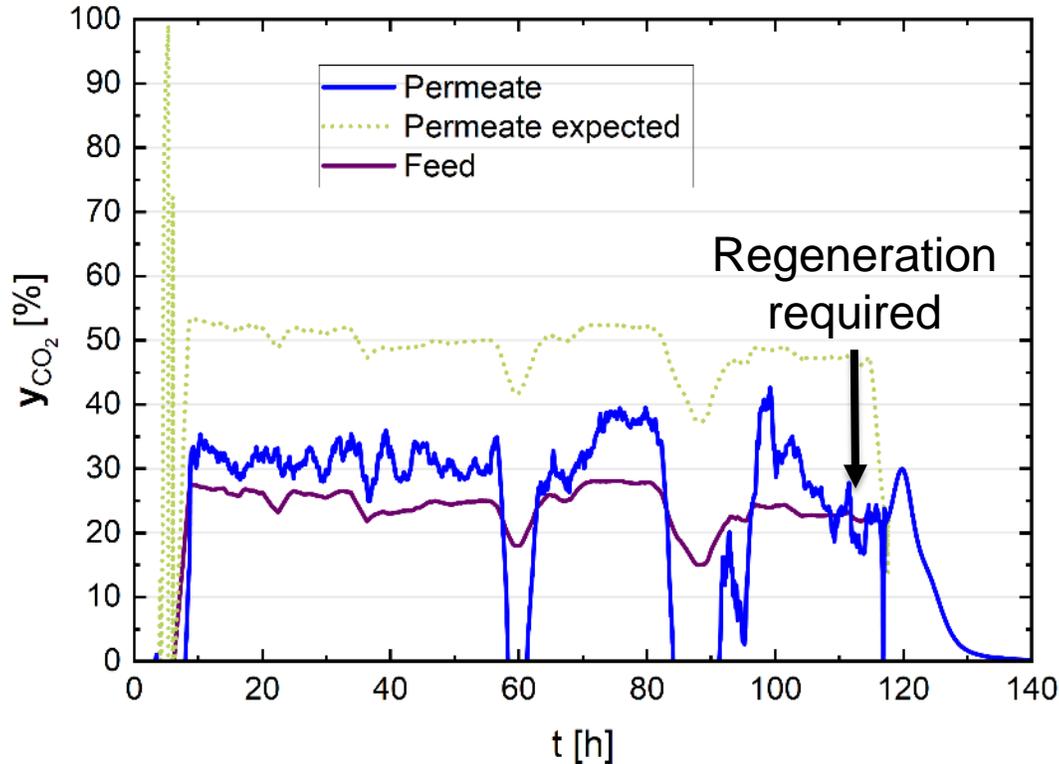
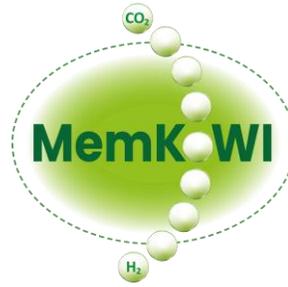
Module 1 – polymer membrane:

- CO₂ selective PolyActive™
- Area A_M = 16 m²
- Selectivity α_{CO₂/N₂} (ϑ = 25°C) = 47
- Permeance L_{CO₂} (ϑ = 25°C) = 3 Nm³/(m² h bar)
- Up to V_F = 80 Nm³/h

Module 2 – ceramic membrane:

- CO₂ selective α-Al₂O₃+8YSZ+Carbon
- A_M = 0.96 m²
- α_{CO₂/N₂} (ϑ = 20°C) = 20
- L_{CO₂} (ϑ = 20°C) = 1 Nm³/(m² h bar)
- Up to V_F = 8 Nm³/h

1st Operating performance single stage mode – ceramic membrane



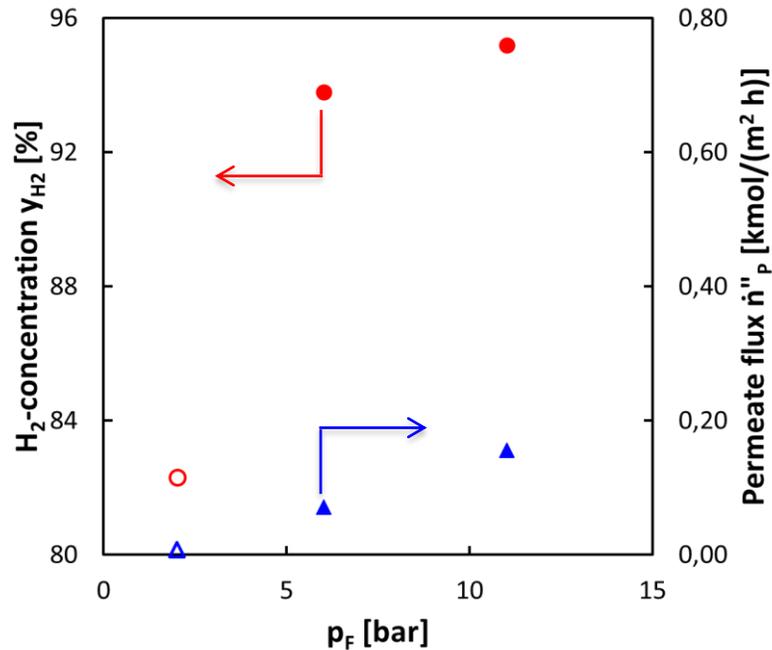
Observations:

- ceramic module performance degrades fast in flue gas
- permeance and selectivity influenced by water and flue gas components
- lab-regeneration at $\sim 400^{\circ}\text{C}$ successful ... \rightarrow again fast degradation in industrial environment
- \rightarrow **Ceramic membrane less successful for CO_2 -separation compared to polymer membrane**

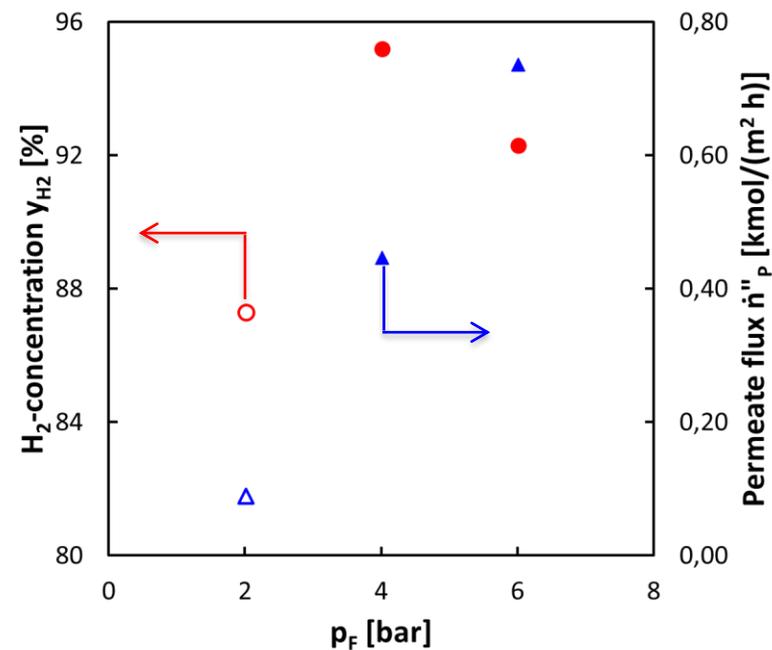
H₂ separation

- H₂ separation from COG & BFG (*finalizing construction for commissioning in Dec. 2025 – fit for 180°C*)
- COG with $y_{F,H_2} = 56\%$ (synthetic gas mixture, ideal conditions)
- **Lab-scale trials** with MemKoWI-membranes at BFI

Polymer membrane (Hereon)



Ceramic membrane (FZ Jülich)



Observations:

→ Membranes well suited for H₂ separation from COG

→ **Ceramic membrane clearly outperforms polymer membrane:**

→ Higher fluxes at lower pressures with nearly identical H₂ purity

Results and next steps



■ Results:

- **Achieved CO₂ separation:** > 50% CO₂-off-gas depletion & >95% CO₂-Permeat for use (CCU) ✓
- **Long-term operation** of polymer & ceramic membranes in industrial gas:
sensitive to specific fluctuations (acid gases and water vapour) ✗
 - risk mitigation possible by automated process control with Polymer membrane ✓
 - regeneration possible for ceramic membranes ✓
 - stable high long-term performance with polymer membrane for CO₂-separation ✓ → for further upscaling & CCU simulation tool: operating performance predicted ✓
- **Findings used for adapted concepts** and layout of the **further pilot plants** for: ✓
 - H₂ separation from COG & BFG (*finalizing construction for commissioning in Dec. 2025 – fit for 180°C*)
 - CO₂ separation from BFG, cement plant- and biomass power plant-flue gases (*finalizing optimized constructions*)

■ Next steps:

- **Long-term-testing** other gas-membrane-combination with modelling & optimization & evaluation of potential for TRL9
- **Membrane type- & module-upscaling** based on pilot trial experiences
- **New pilot plants** commissioning, testing and optimisation under industrial conditions
- **Develop upscaling concepts** with cost and potential for CCU & CCUS

Power4Steel with MemKoWI

Thank you! → Questions?

Power4Steel



Commissioning MemKoWI-pilot plant at Dillinger



MemKoWI-meeting in Dillingen - plant tour with Power4Steel



MemKoWI-Project coordination

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<p>Research</p> <p>Membranes/Polymer</p> <p>Membranes/Ceramic</p>	<p>Steel industry</p> <p>Bfi Angewandte Spitzenforschung</p> <p>Gas technologies</p>	<p>Steel industry</p> <p>DILLINGER</p>	<p>Cement industry / Plant design</p> <p>thyssenkrupp Polysius</p>
<p>Membrane production</p> <p>atech innovations gmbh</p>	<p>Regenerative energies</p> <p>iqony</p>	<p>Engineering</p>	

Power4Steel-Project of Dillinger-SHS-Saarstahl

our path to "green steel":
Power4Steel our journey – **Pure Steel+** our destination

follow our progress:
www.pure-steel.com



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