

# ESTEP SPRING DISSEMINATION EVENT

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Synergies between RFCS  
Projects on Hydrogen  
application in the  
Blast Furnace process

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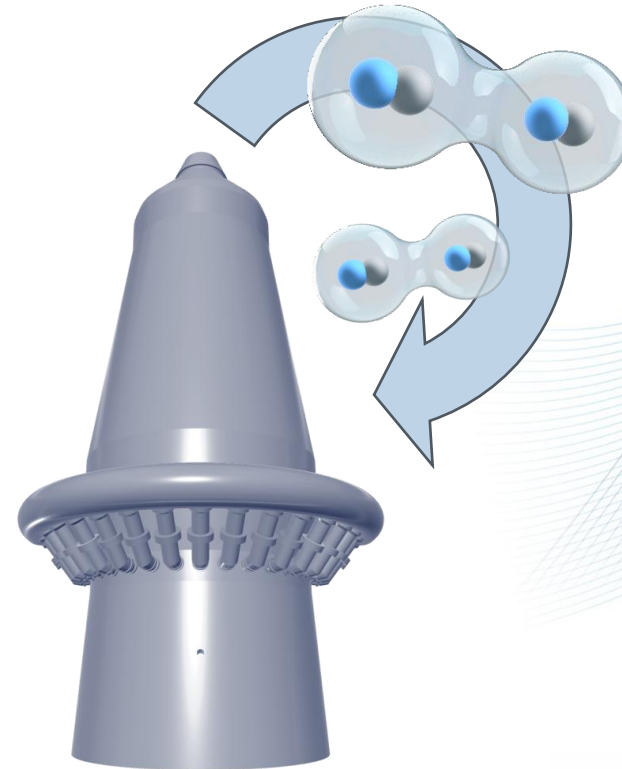


# Synergies between RFCS Projects on Hydrogen application in the Blast Furnace process

- **H<sub>2</sub>TransBF 2030**  
(2022 - 2025)
- **H<sub>2</sub>II**  
(2024 - 2027)
- **H<sub>2</sub>loop**  
(2025 - 2028)



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## CO<sub>2</sub> Emission target boundary conditions for steel production

- › To mitigate global warming the EU has set targets to reduce CO<sub>2</sub> emissions by 55% until 2030 and to become carbon neutral until 2025.
- › Until 2025 the steel sector receives free CO<sub>2</sub> emission certificates following a benchmark system.
- › Carbon Border Adjustment Mechanism (CBAM) will start in 2026, in parallel new benchmarks for CO<sub>2</sub> emission certificate allocations to the steel industry will be set up.
- › With the ramp-up of CBAM after 2026, it is foreseen to reduce the amount of freely allocated certificates.
- › CO<sub>2</sub> Emission certificate prices in average were around 65€ in 2024.
- › The steel industry requires solutions to reduce CO<sub>2</sub> emissions at short notice
- › Application of Hydrogen to the Blast Furnace has been demonstrated to be technical solvable and is reported to have a CO<sub>2</sub> Emission reduction potential of up to 20% technically



# Questions to be answered to optimise the Hydrogen use in the BF process

- › What are optimal BF operational conditions to maximise CO<sub>2</sub> mitigation?
- › How can Hydrogen be injected into the BF to maximise the gas utilisation?
- › How can Hydrogen be produced on site considering fluctuating energy prices and stepwise site transformation?





# What are optimal BF operational conditions to maximise CO<sub>2</sub> mitigation?

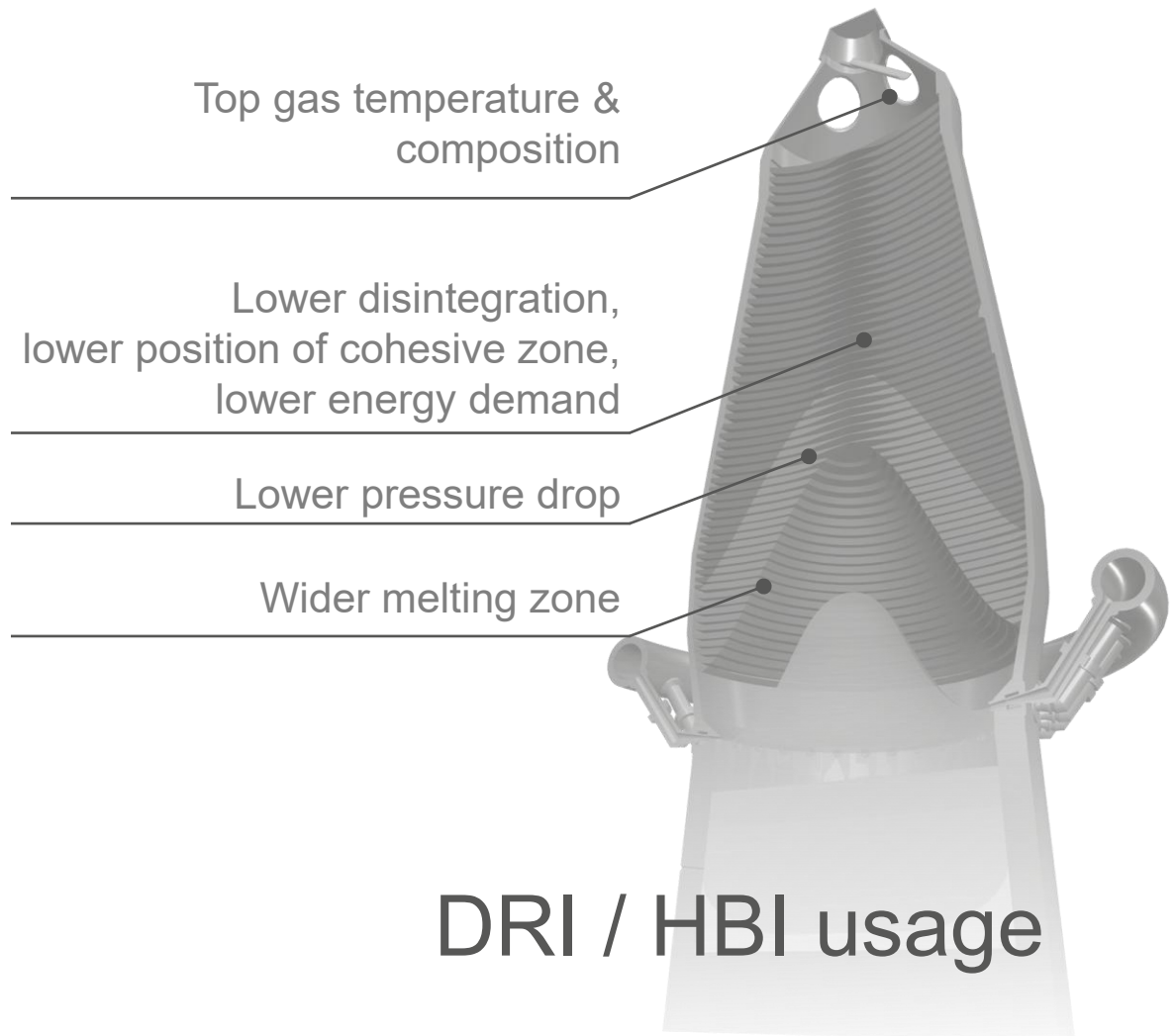
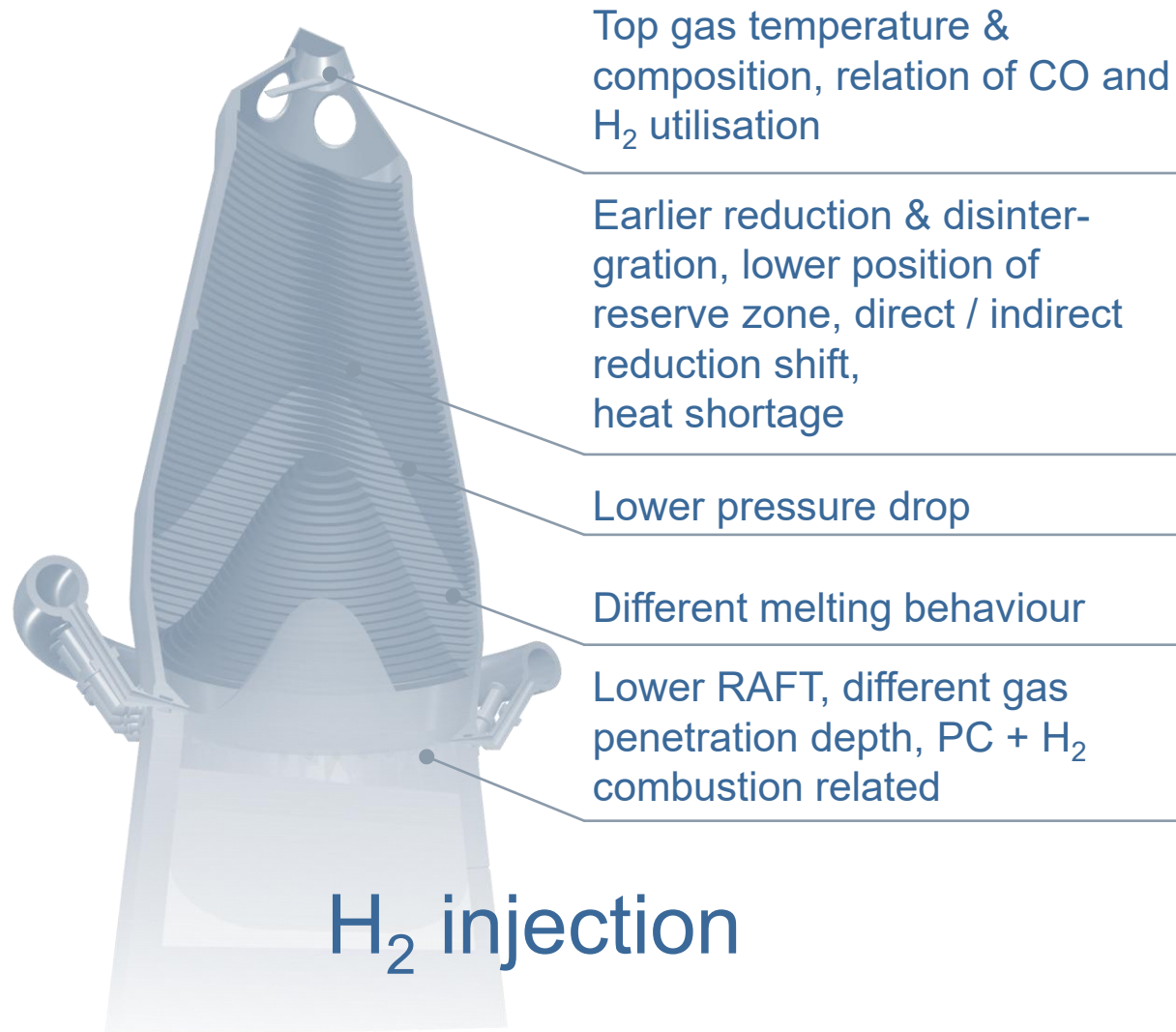


Minimisation of CO<sub>2</sub> Emissions from the BF by hydrogen containing injectants and use of DRI/HBI during transition to new Ironmaking processes until 2030

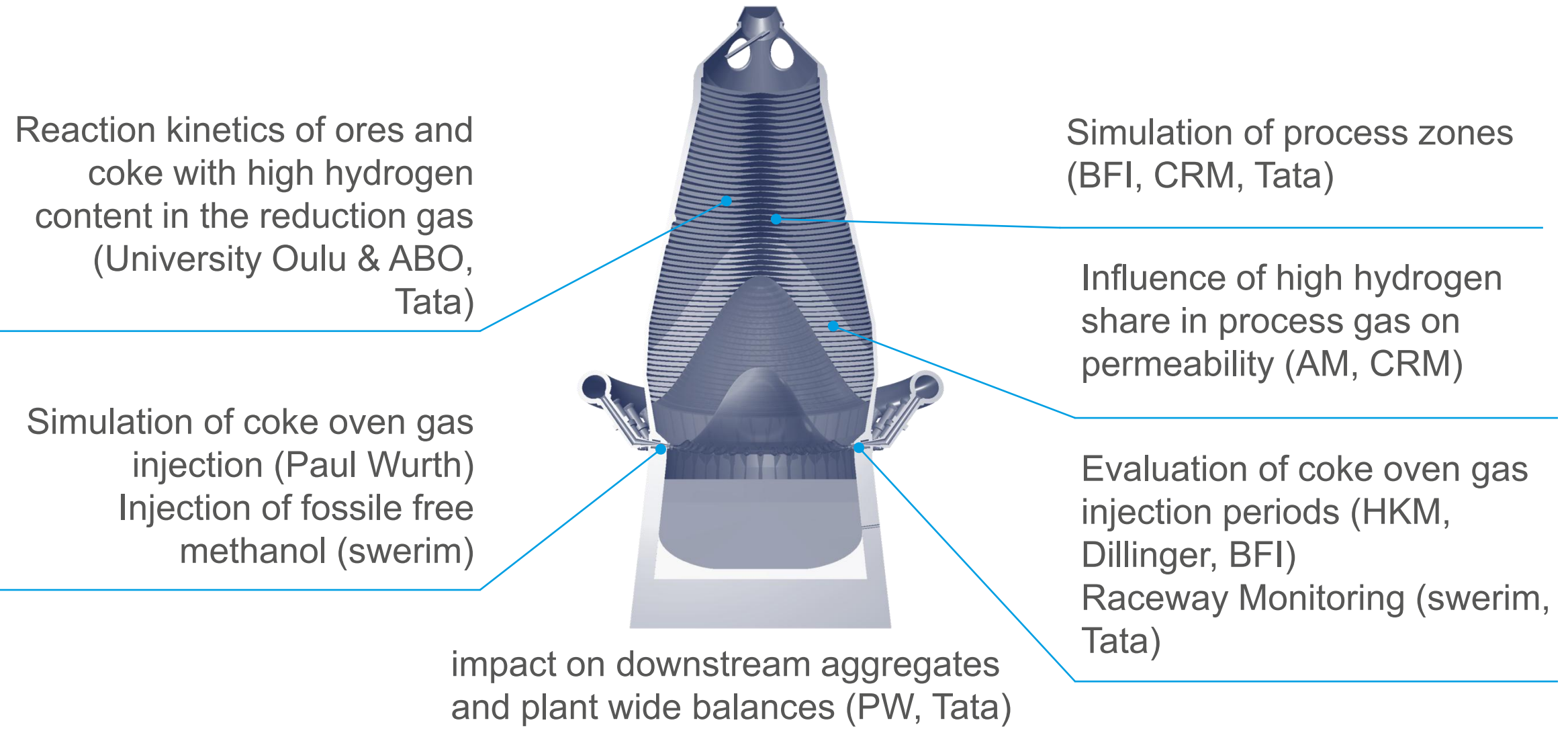


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# Knowledge about influence of H<sub>2</sub>-Injection and use of DRI/HBI on the BF process

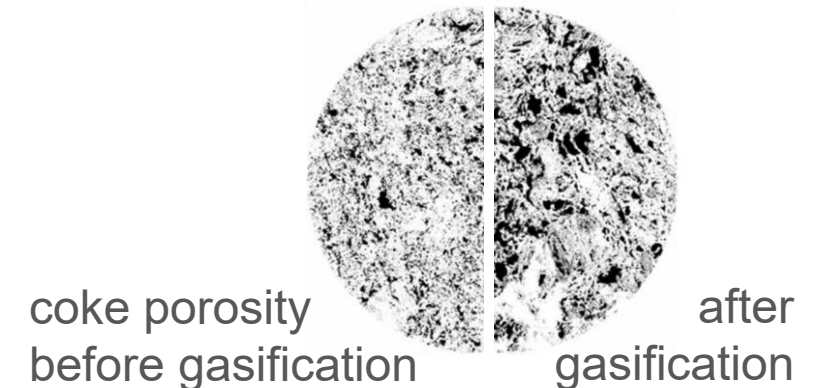
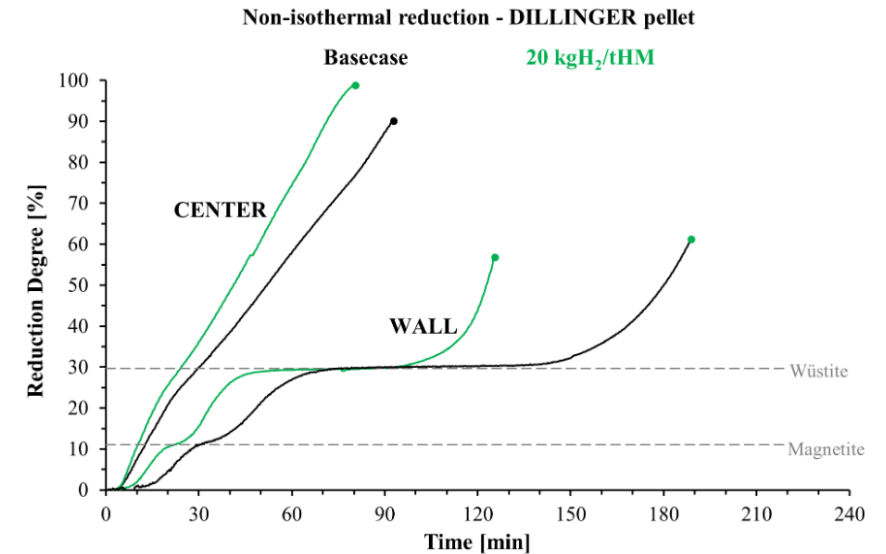


# H2TransBF2030 - Project focus and activities



# Results (1) - Impact of higher hydrogen content in the reduction gas on ore and coke (Oulu University)

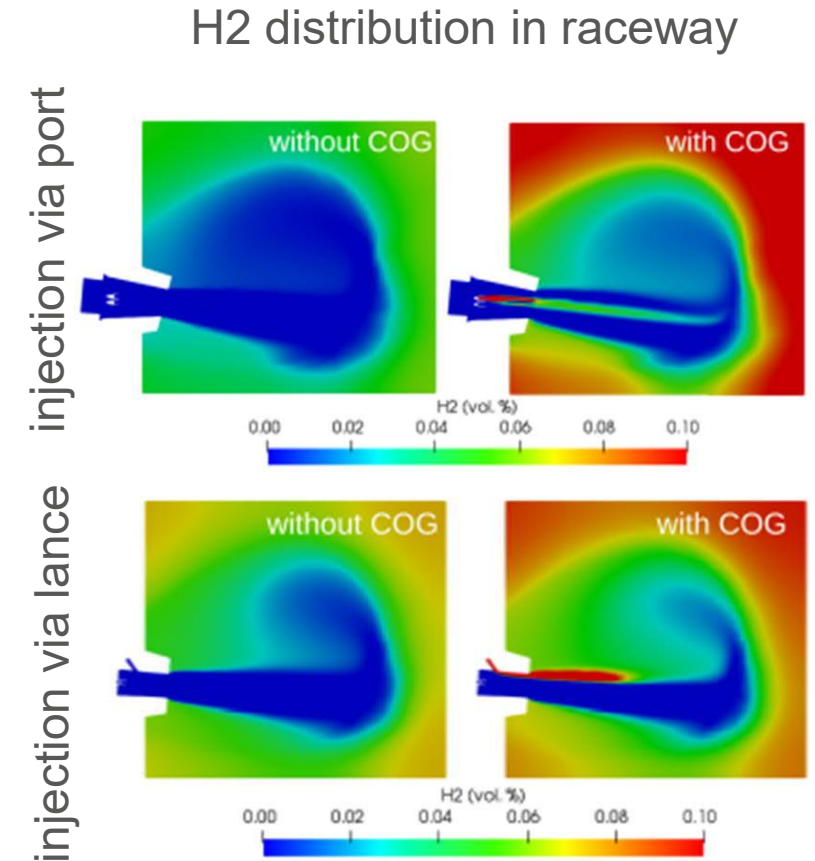
- › Hydrogen injection enhances initial reduction rate - its overall impact varies by temperature. At 700 °C the reduction with hydrogen sometimes plateaus at lower final values, while at 900 and 1100 °C, it generally expedites the formation of metallic iron.
- › SEM-EDS analyses show that the sample periphery typically undergoes reduction earlier and exhibit greater pore development than the core. Pellet porosity exhibits almost linearly with reduction degree in isothermal reduction.
- › According to combined results of carbon conversion and porosity development during the gasification of coke, it is suggested that water and hydrogen in the system promote surface reaction, which may cause issues with the BF operation.



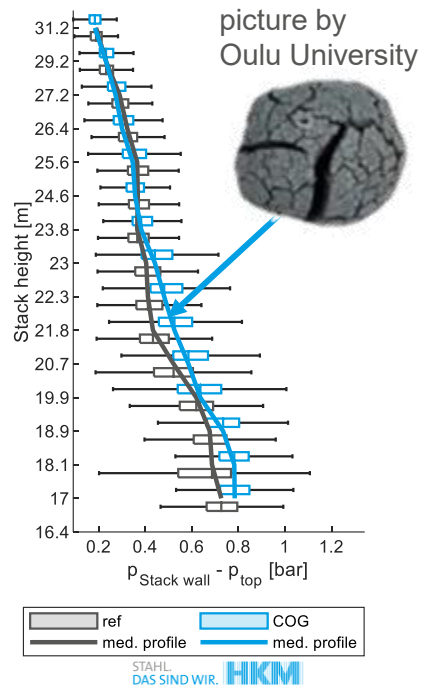
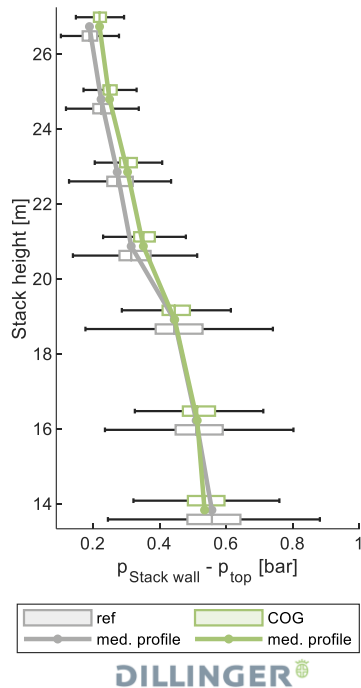


## Results (2) - Injection of hydrogen containing gases (Paul Wurth)

- › COG increases the blast velocity at tuyere nose.
- › The combustion of pulverized coal can be enhanced by improving the mixing between PCI plume and COG jet.
- › Oxygen levels must be adjusted to maintain combustion stoichiometry and RAFT.
- › With COG co-injection, the gases exiting the raceway become richer in H<sub>2</sub> (higher production of H<sub>2</sub>O compared to CO<sub>2</sub> in the raceway, faster reaction rates of steam gasification)
- › If COG is injected via port, the rate must be sufficient to ensure good penetration into the blast. If COG is injected via lance, it may impose additional heat loads on the tips of the lances.

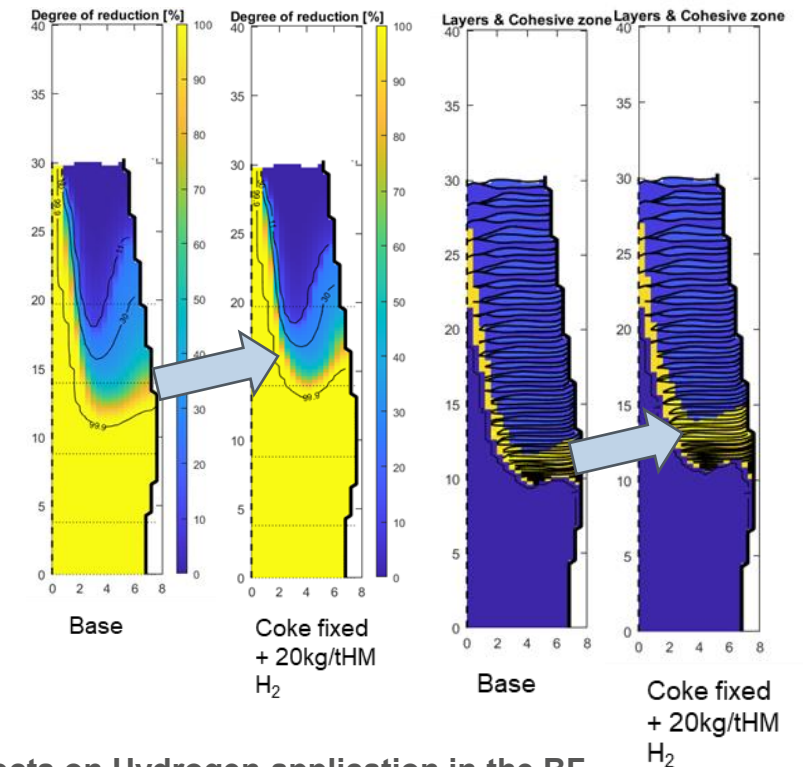


# Results (3) - Impact of higher hydrogen content in the reduction gas on process zones (HKM, Dillinger, BFI, Tata)



COG injection of 8.000 m<sup>3</sup>/h at Dillinger resp. 22.000 m<sup>3</sup>/h at HKM

- › increased pressure drop from hot blast to top,
- › but a more even distributed pressure drop of the process gas during passage of the burden column especially in the cohesive zone,



Simulation of normal operation vs. 20kg<sub>H2</sub> / t<sub>HM</sub>

- › faster start of reduction
- › wider cohesive zone

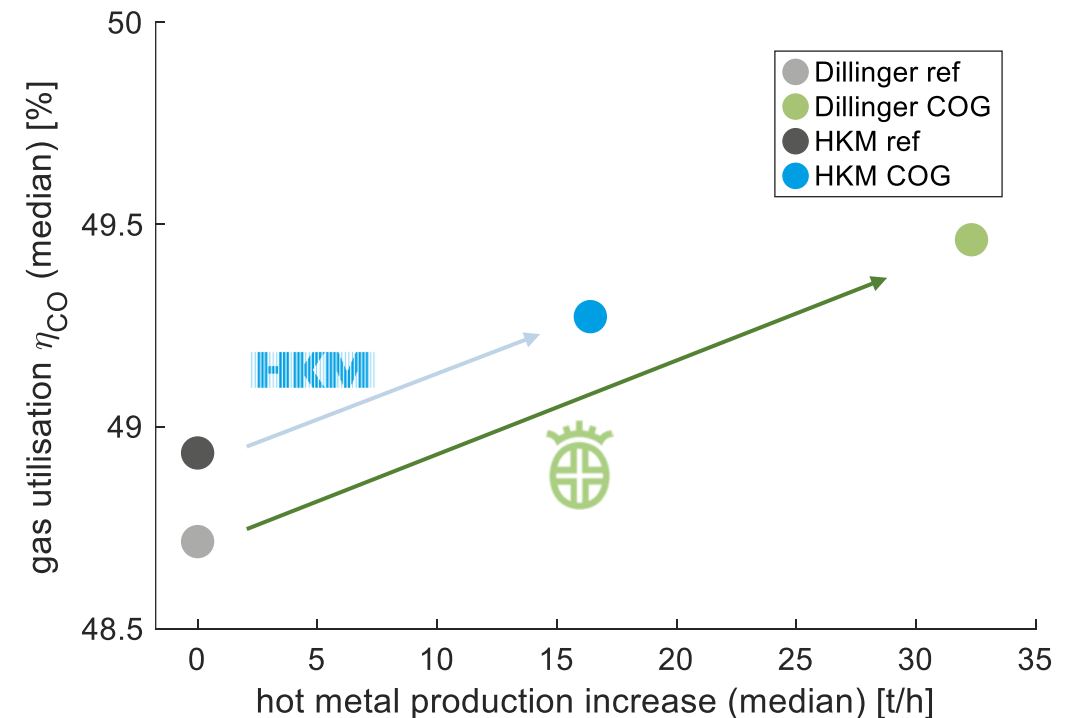
## Conclusions so far

Coke oven gas injection is beneficial for the BF

- › earlier start of reduction enables higher productivity
- › gas utilisation of carbon monoxide is increased

Attention must be paid to

- › process requires optimisation of working point (replacement of coke / coal, charging pattern)
- › Monitoring of permeability due to possible material degradation at lower temperatures



# How can Hydrogen be injected into the BF to maximise the gas utilisation?



Hydrogen sequence impulse injection  
into the Blast Furnace shaft



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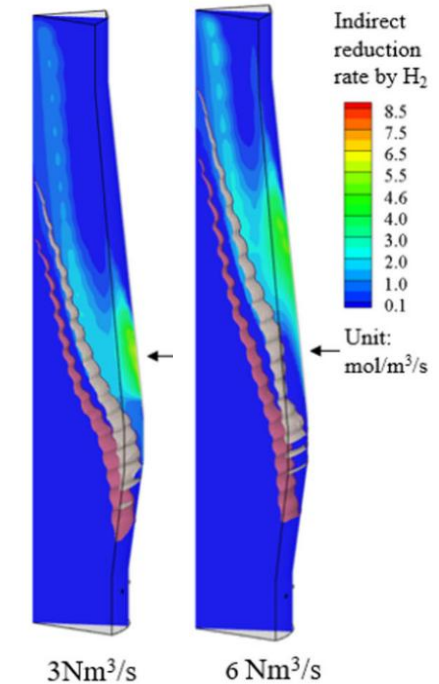




# Impulse injection of hydrogen – State of the art

## › State of the art

- › Hydrogen reduction can save up to 20% of the CO<sub>2</sub> emissions of a blast furnace
- › Hydrogen achieves higher reduction rates already at lower temperatures than CO (from approx. 800-900°C).
- › Due to the low density of the hydrogen gas, it is difficult to achieve high penetration depths (applies to blast furnaces, but also direct reduction plants)
- › Pulse injection technology with Oxygen at tuyere level has shown higher penetration depths and better shaft gas flow in industrial application



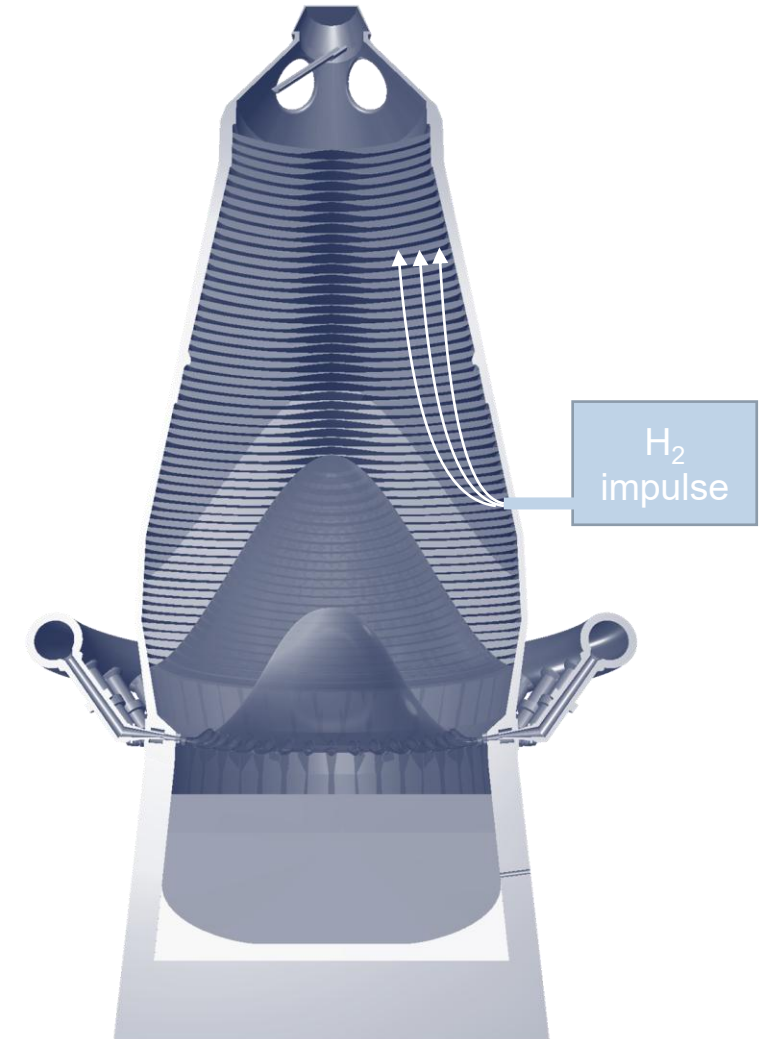
Li, J. et al. Numerical modeling and analysis of hydrogen blast furnace ironmaking process. Fuel 323, 124368 (2022).



## Why pulse shaft injection and not injection via tuyeres?

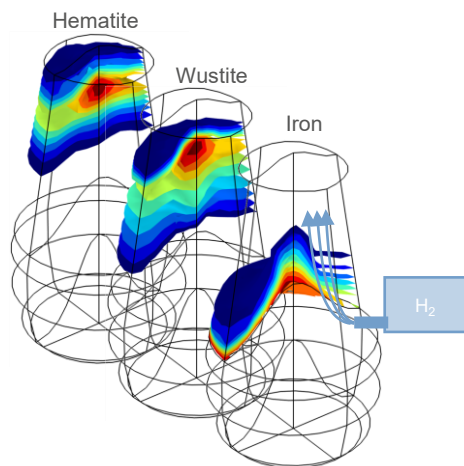
### › Challenges of H<sub>2</sub> tuyere injection

- › **Reaction Kinetics** - H<sub>2</sub> reacts more rapidly than coal with available oxygen, potentially reducing coal conversion efficiency.
- › **Flame Characteristics** - H<sub>2</sub> combustion is highly exothermic, generating extremely high temperatures at lance tip and tuyere. Upon reaching the coke bed, H<sub>2</sub>O vapor reacts with coke in an endothermic reaction.
- › **Gas Utilisation** - A portion of the injected H<sub>2</sub> enters the central coke chimney, where little ore is present, resulting in suboptimal gas utilization

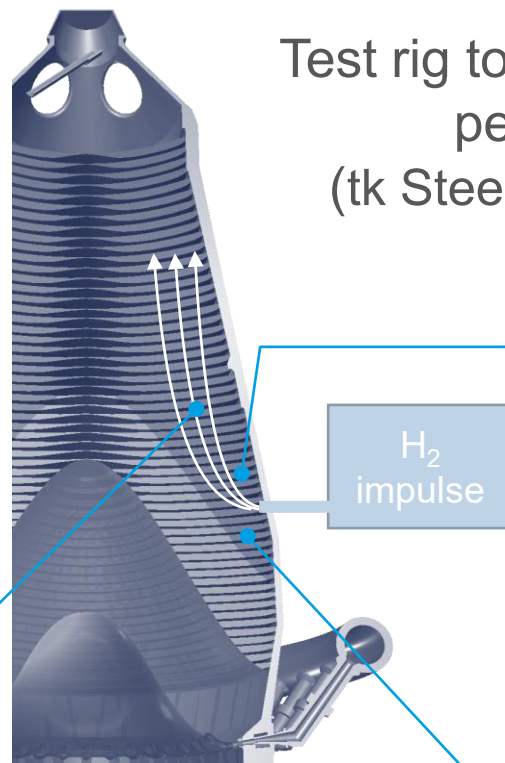




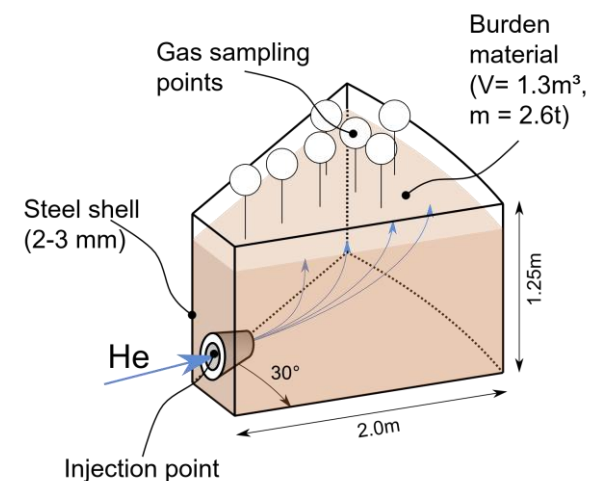
## Project focus and activities



Position of optimal injection level  
and simulation of overall  
process response (BFI)



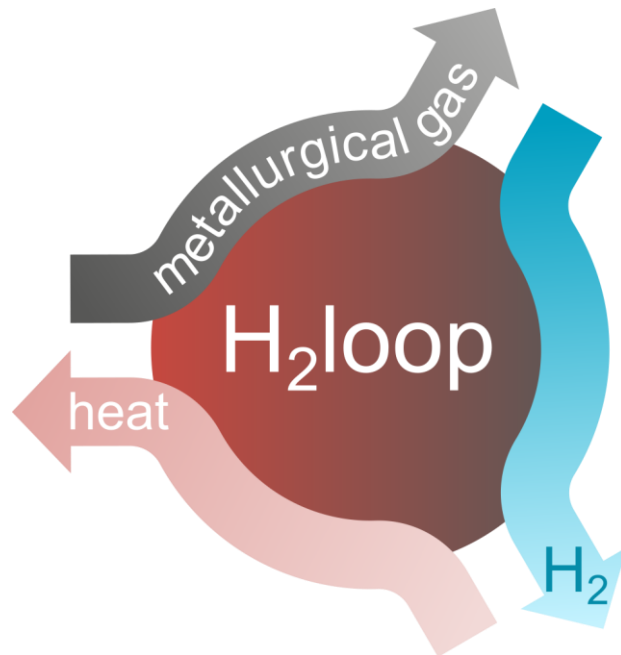
Test rig to examine pulse  
penetration depth  
(tk Steel, tk AT.PRO tec,  
BFI)



Simulation of the  
interrelation between  
pulse and packed bed  
(K1-MET)

Demonstration at an industrial scale BF  
(voestalpine, Primetals, tk AT.PRO tec)

# How can Hydrogen be produced on site considering fluctuating energy prices and stepwise site transformation?



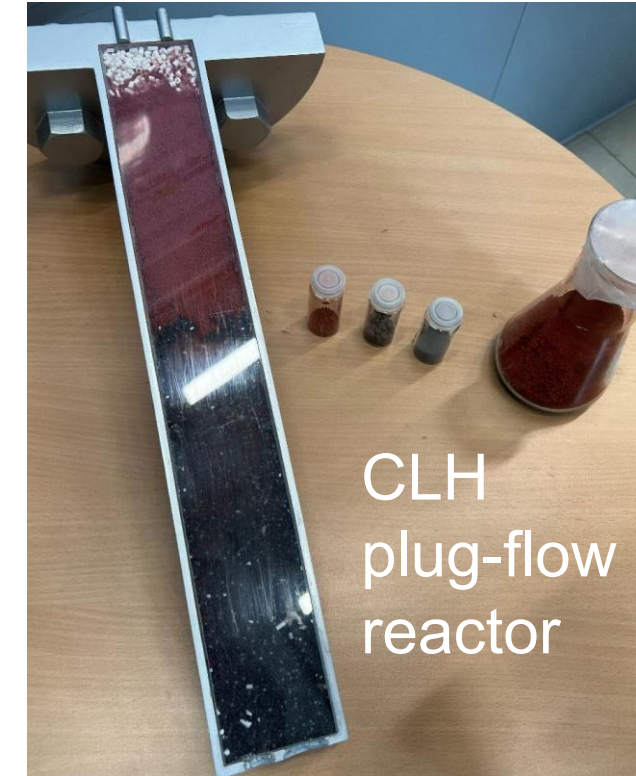
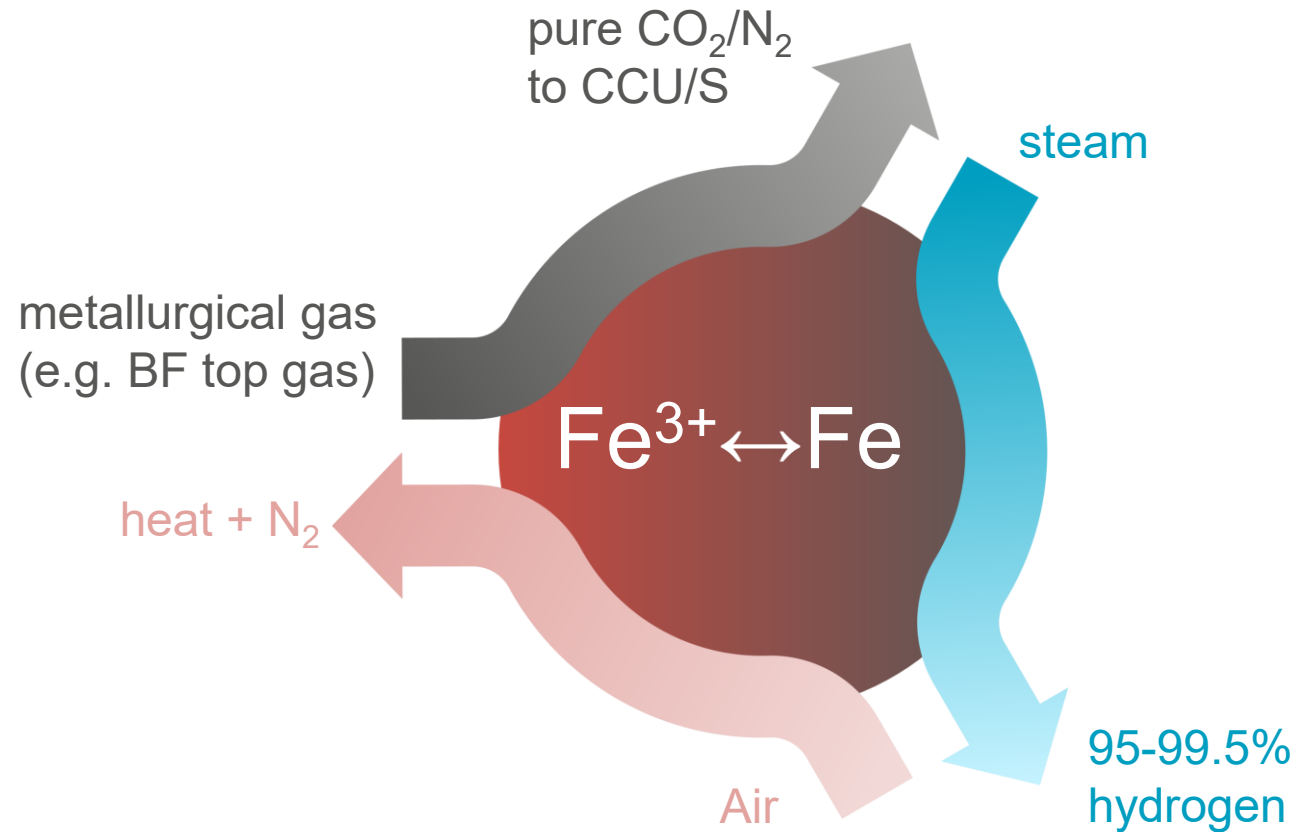
Sustainable decarbonisation of integrated steel plants by hydrogen production from chemical looping (H<sub>2</sub>Loop)



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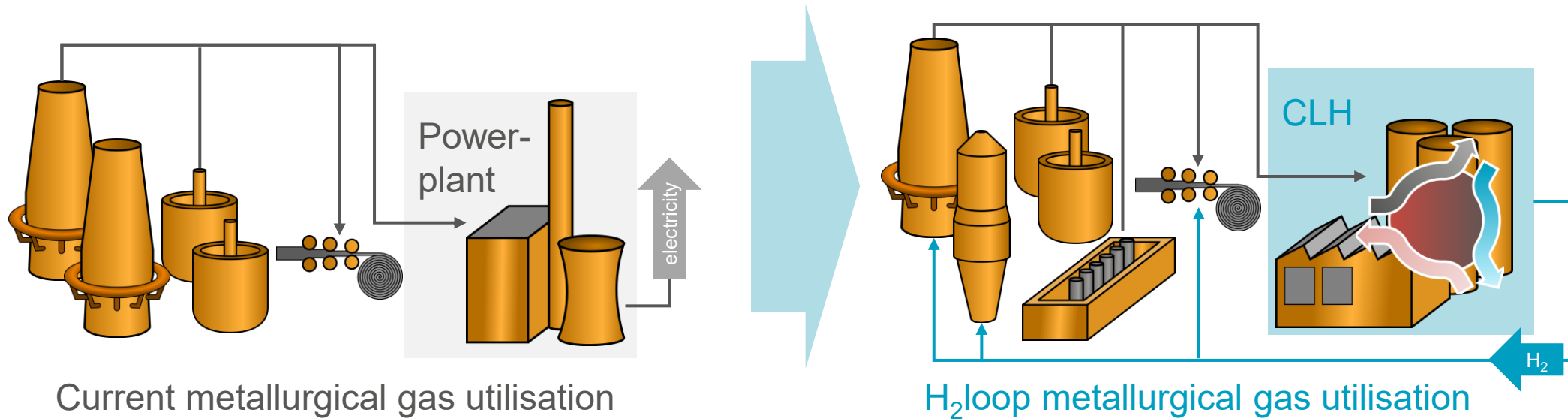


# Project core | The chemical looping hydrogen Process



The CLH process passes through three process stages (i) reduction of oxygen carrier by metallurgical gas, (ii) production of hydrogen from steam and (iii) recovery of rest oxidation potential to supply heat

# Integration scenario for chemical looping process

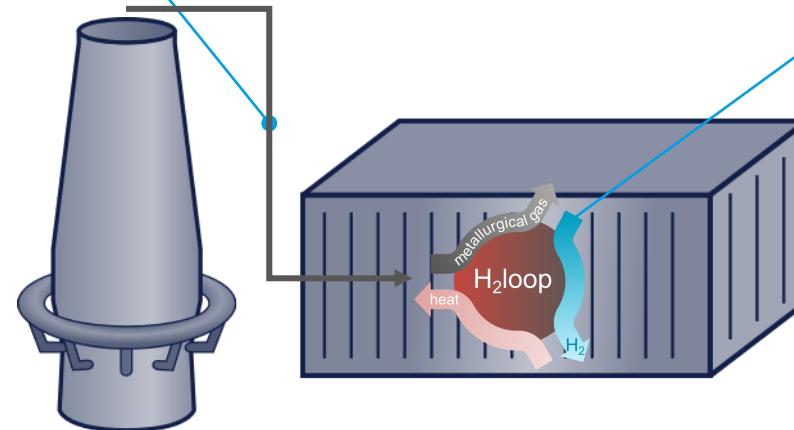


Due to the possibility to use metallurgical gases and to supply hydrogen the CLH process has a high integration potential into current and future steel plant layouts

# Project focus and activities

pilot- and demonstration  
scale on-site tests  
(RGH2, ADI)

Test with a variety of different  
gases from steelmaking, digital  
twin of the chemical looping  
process (BFI)



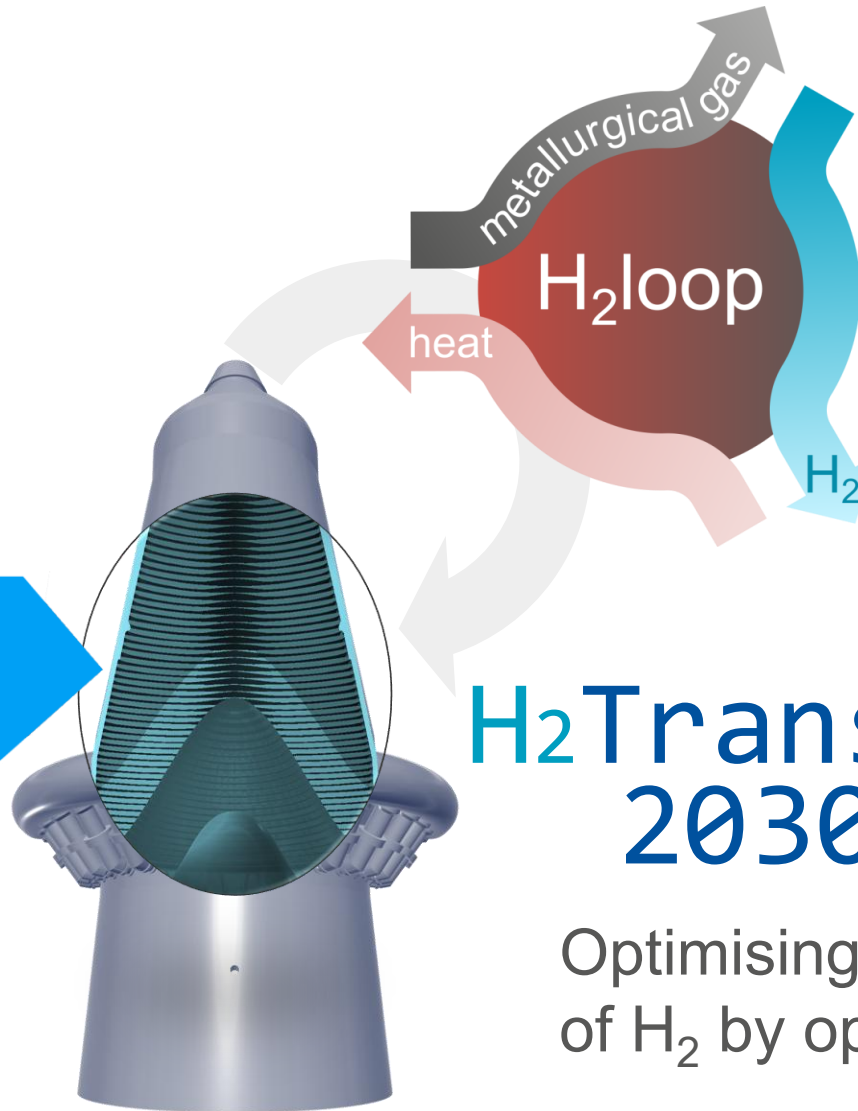
Integrability in different sites layouts, holistic evaluations including LCA and consideration of relevant boundary conditions as e.g. the development of energy markets (PoliTO)

# Summary : three RFCS projects – one holistic concept – multiple synergies

Hydrogen sequence  
impulse injection  
into the Blast  
Furnace shaft

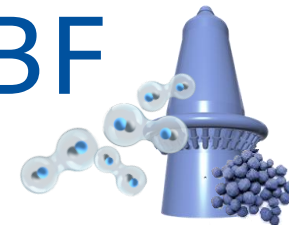


Optimising H<sub>2</sub> usage by  
pulse injection



Enhancing  
efficiency of H<sub>2</sub>  
generation and  
top gas utilisation

H<sub>2</sub>TransBF  
2030



Optimising CO<sub>2</sub> reduction potential  
of H<sub>2</sub> by optimal BF work-points





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<http://h2transbf2030.org/>



<http://h2ii.org/>



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