

# ESTEP SPRING DISSEMINATION EVENT

5-6 JUNE 2025 KRAKOW (POLAND)

Turning biowaste into **steel-grade biocoal** to decarbonize the steelmaking process

Andrea Salimbeni  
Head of Unit, RE-CORD

**Bio**  
RECAST



**H2Steel**



HOTEL ★★★  
**GALAXY**  
JORDAN GROUP

**Łukasiewicz**  
GIT

# 1<sup>st</sup> Challenge: Decarbonizing the EU steel sector

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136 Mt/y  
Crude steel  
produced

56 Mt/y  
fossil coal  
consumed

183 Mt/y of CO<sub>2</sub> emitted<sup>1</sup>

(5% of EU GHG Emissions)

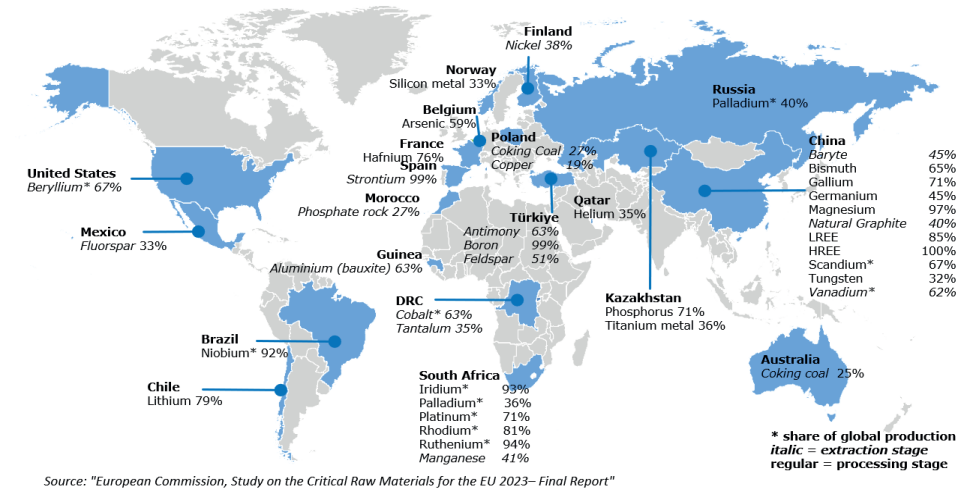


EU ETS regulation – “Polluters pay”  
principle

<sup>1</sup>EU JRC Technical report – Greenhouse gas intensities of the EU steel industry and its trading partners, 2022



# 2<sup>nd</sup> Challenge: waste recycling



## EU Critical Raw Materials Act

at least 15% of the EU's annual consumption for recycling

Sludge  
11 Mil dt/y

OFMSW  
40 Mil dry t/y

# Objectives

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## **Main goal**

Use biogenic residues to produce biocoal for steel sector



## **Challenge**

Waste streams contains not only in carbon, but also in inorganic contaminants not extracted by conventional processes



## **Proposed solution**

Integrated process based on thermochemical treatment and chemical leaching

# RFCS PROJECT- BIORECAST

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## BioRECAST

“BIObased RESidues Conversion to Advanced fuels for sustainable SSteel production”.

## RFCS funded project

11/2023 – 04/2027



Funded by  
the European Union

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DIPARTIMENTO DI MECCANICA



# TRANSINTER PROJECT

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## TRANSinter

“Valorisation of the sinter plants to support the transition towards Direct Reduction route”.

RFCS funded project

07/2023 – 12/2026



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the European Union

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# H2STEEL PROJECT

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## H2STEEL

“Green H2 and circular bio-coal from biowaste for cost-competitive sustainable Steel”

EIC funded project  
10/2022 – 09/2025



Funded by  
the European Union

Funded by the European Union - European Innovation Council - H2STEEL project - Grant Agreement nr.101070741. Views and opinions expressed are however those of the author(s) only and do not necessarily reflect those of the European Union or the European Innovation Council.



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“G.Ferraris”



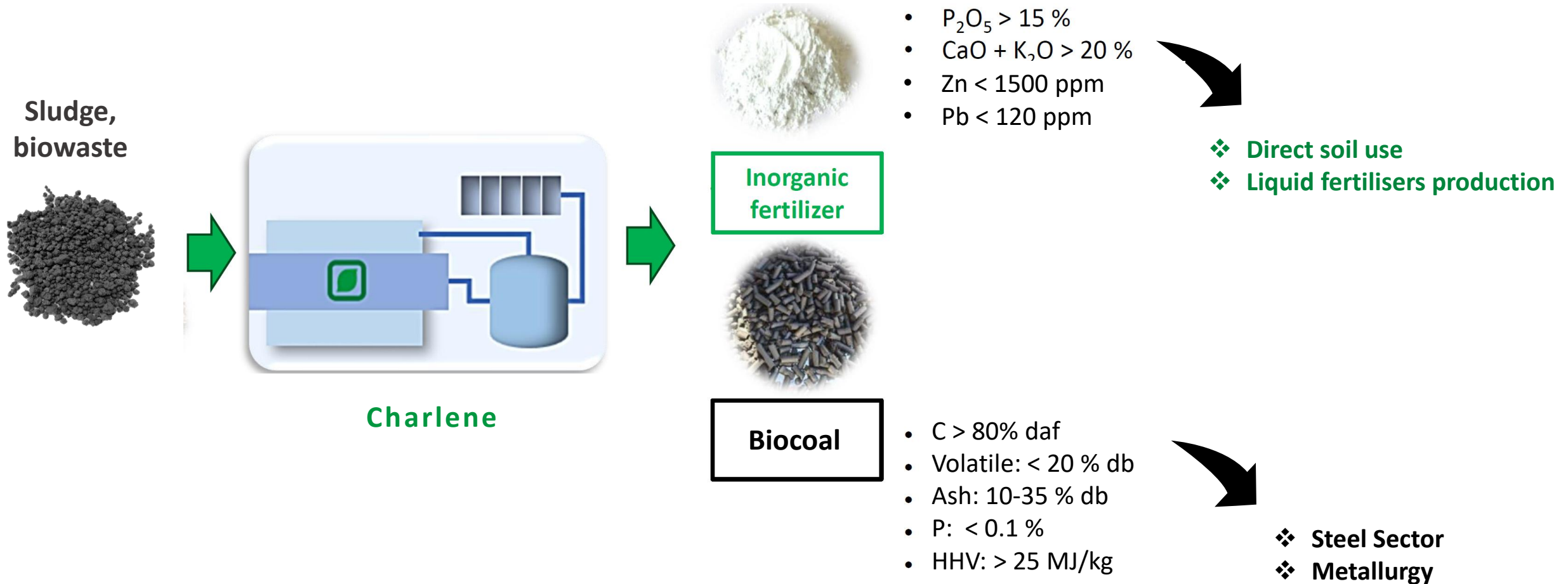
Imperial College  
London



Universiteit  
Leiden  
Institute of  
Environmental Sciences

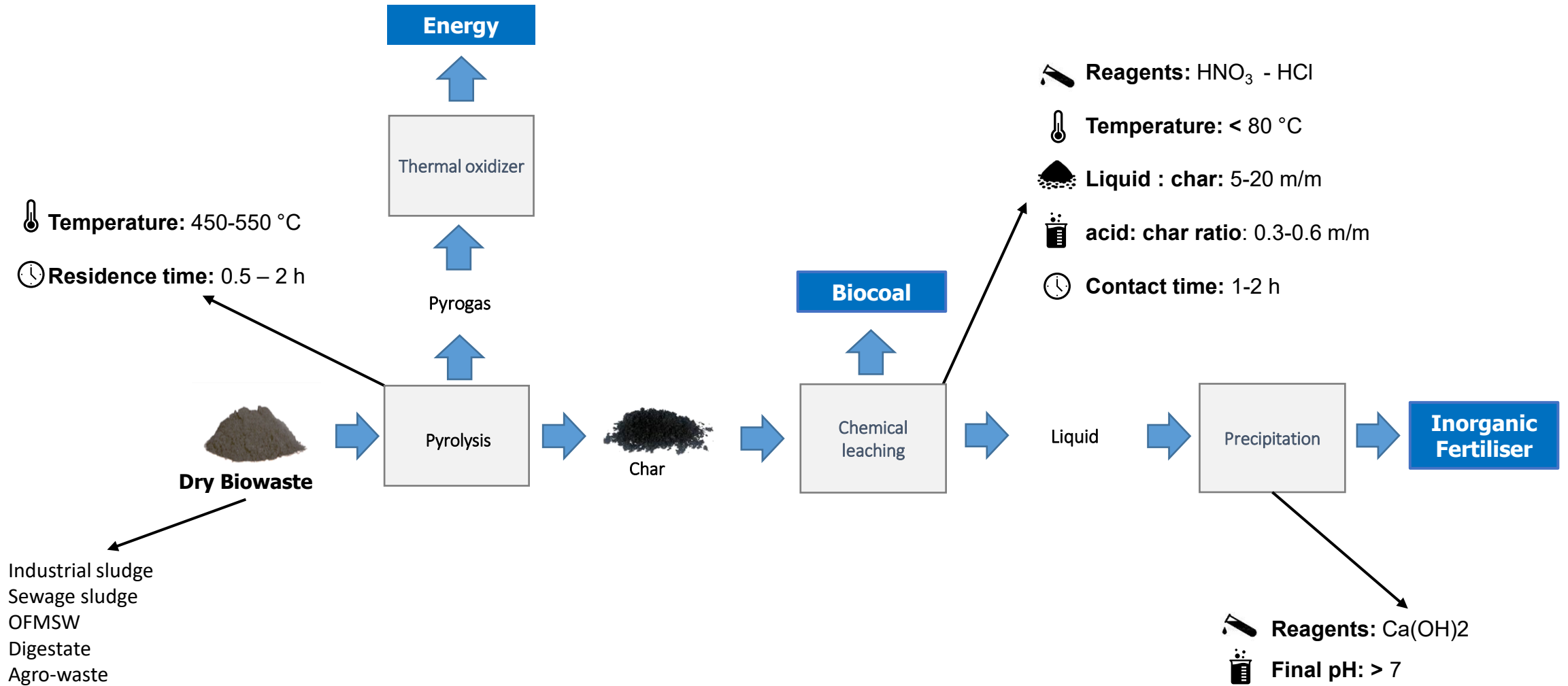


# CHARLENE: Selective recovery process





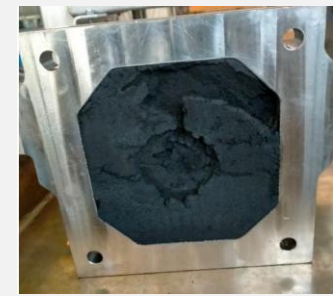
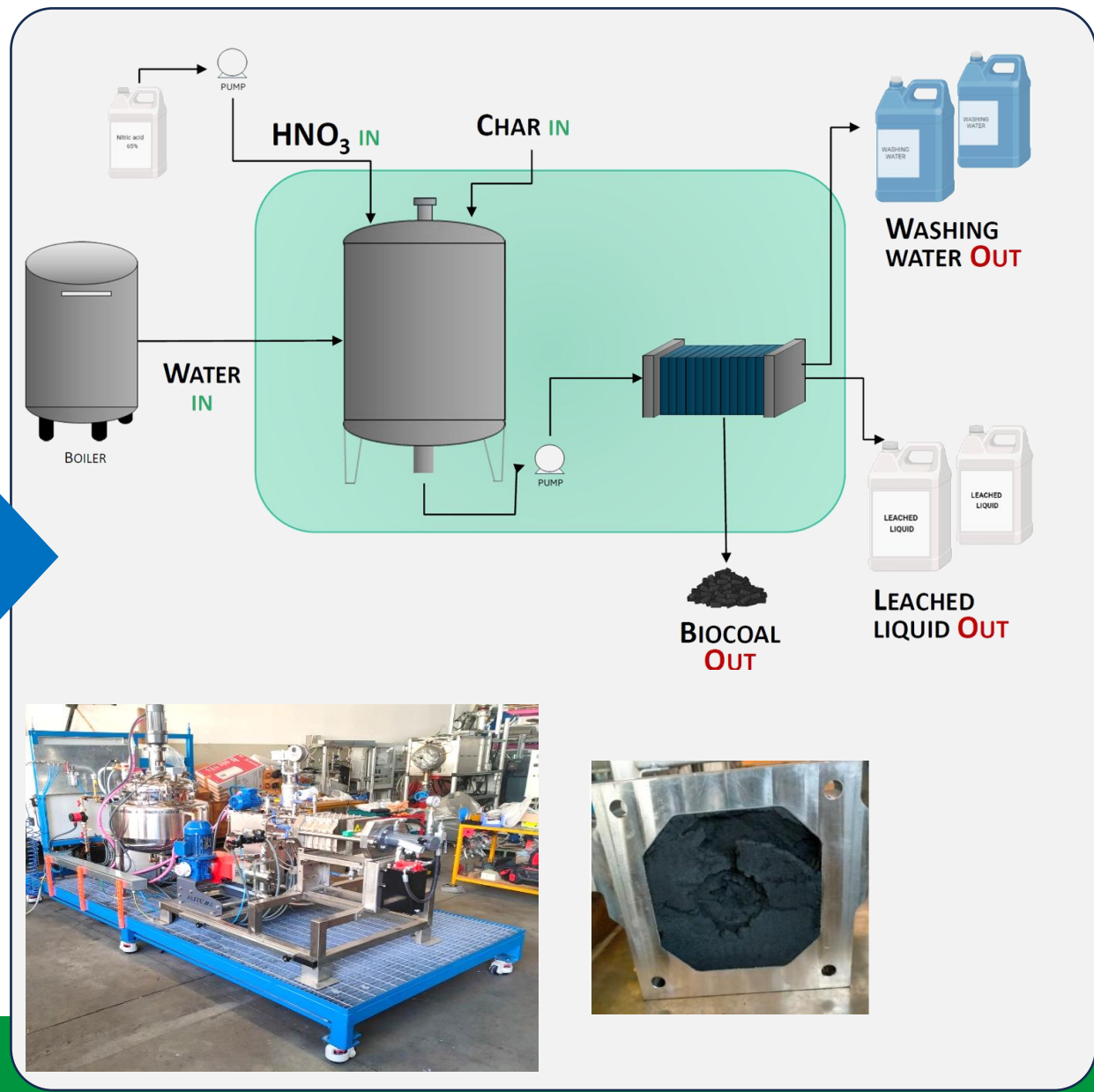
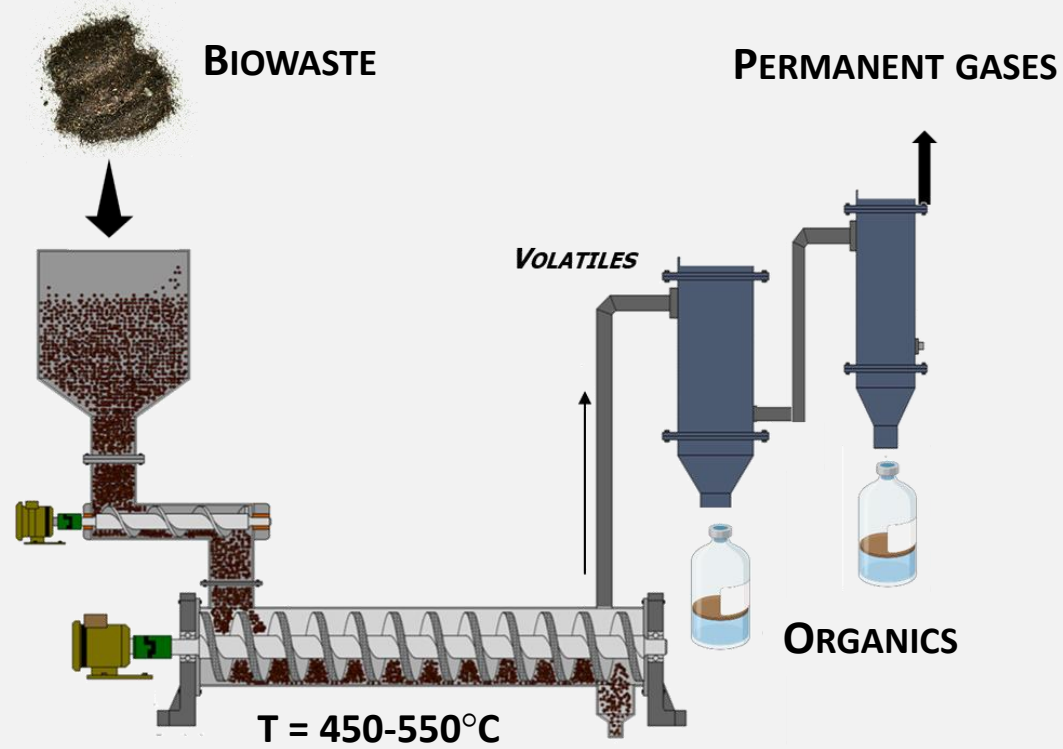
# CHARLENE: Selective recovery solution



# Biocoal production at pilot scale



# METHODOLOGY AND PILOT PLANTS



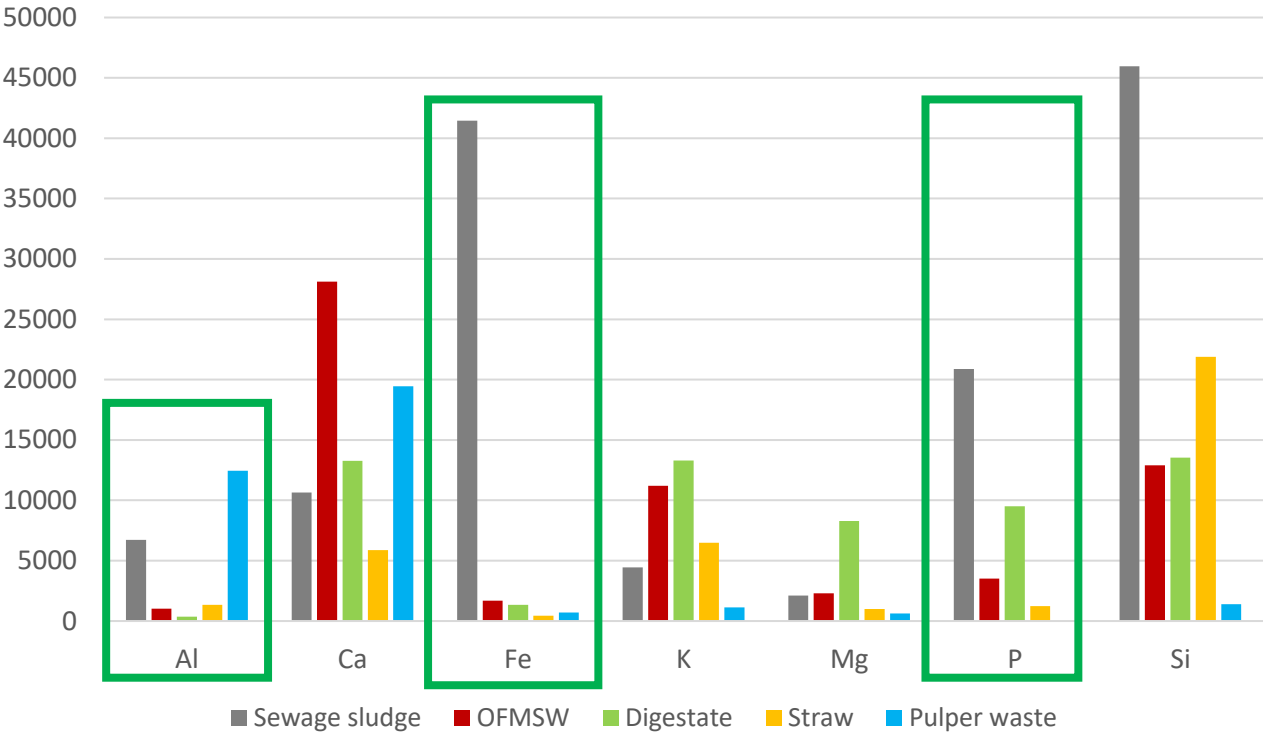


# CHARACTERIZATION OF WASTE STREAMS



Parameter	Sewage sludge	OFMSW	Digestate	Straw	Pulper waste
Ash	27.7%	14.4%	13.8%	8.6%	7.8%
Volatiles	59.2%	71.4%	64.7%	72.7%	82.9%
C	38.0%	44.0%	45.3%	45.3%	63.4%
H	5.3%	5.8%	5.7%	5.8%	8.9%
N	6.6%	1.8%	1.5%	0.9%	0.2%
S	1.0%	0.1%	0.5%	0.1%	0.1%

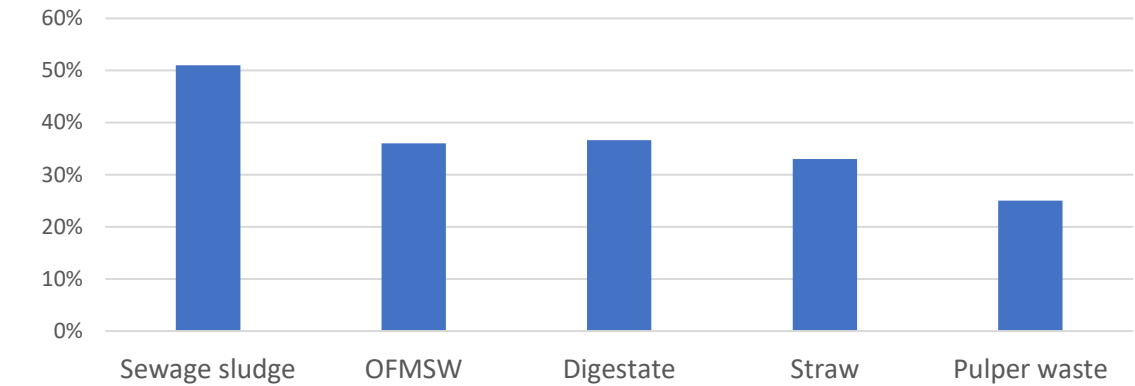
Concentration of inorganic elements



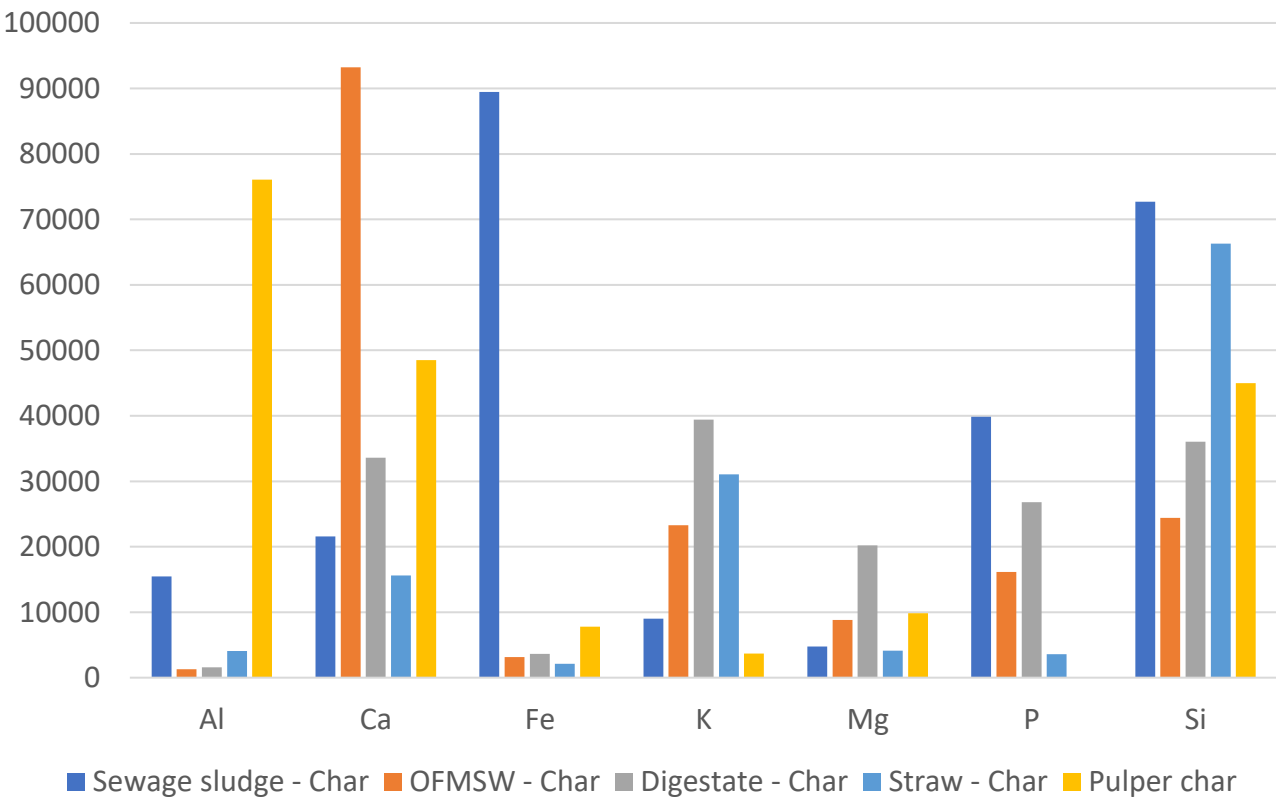
# COMPOSITION OF RAW CHAR AFTER SLOW PYROLYSIS



Char yield (% db)



Concentration of inorganics



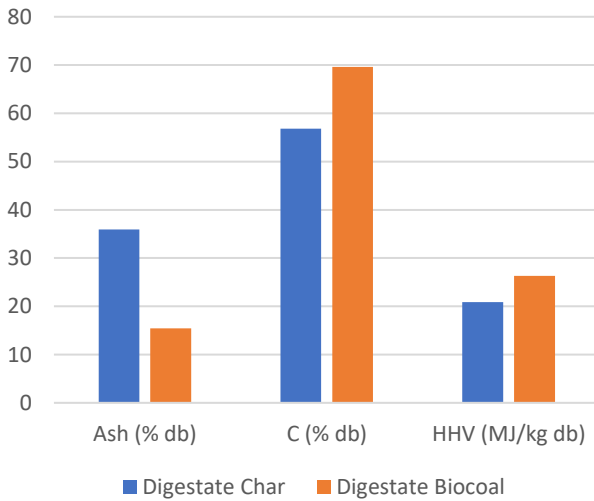
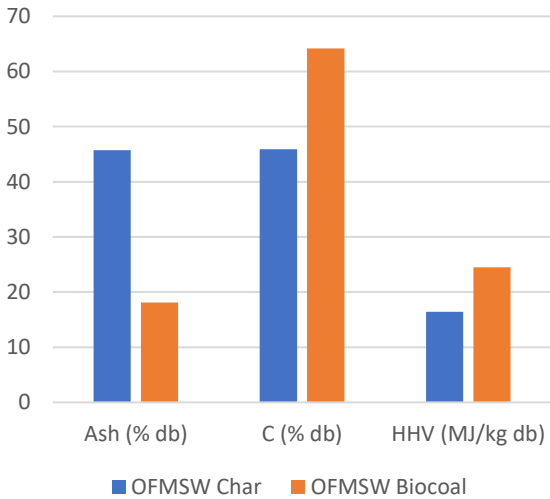
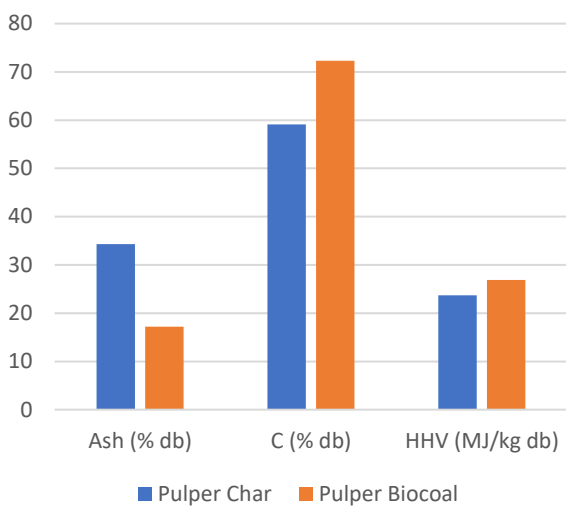
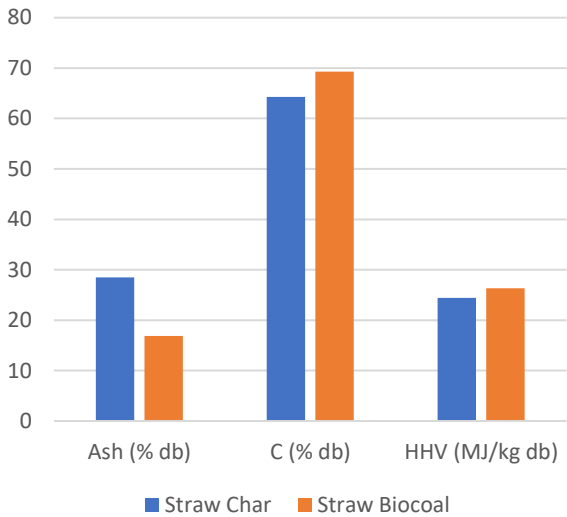
Parameter	Unit	S. Sludge char	OFMSW char	Digestate char	Straw char	Pulper char
Ash	% db	58.4	45.7	35.9	28.5	34.3
Volatiles	% db	17.4	18.1	12	12.2	17.1
C	% db	31.7	45.9	56.8	64.3	59.1
H	% db	1.38	1.3	1.6	2	1.5
N	% db	4.8	2.5	1.5	1.3	0.1
S	% db	0.26	0.2	0.3	0.1	0
Cl	% db	0.76	1.9	0.5	0.5	2.4
HHV	MJ/kg	12.7	16.4	20.9	24.4	23.7

# COMPOSITION OF OBTAINED BIOCOALS



- C content increase of up to 60%
- P reduced to < 0.3%
- Cl reduced to < 0.4%

Parameter	BIOCOAL S. Sludge	BIOCOAL OFMSW	BIOCOAL Digestate	BIOCOAL Straw	Biocoal Pulper
Volatiles	19.5	20.1	18.7	16.9	17.2
Ashes	37.6	18.1	15.4	16.9	14.8
C	42.0	64.2	69.6	69.3	72.3
H	1.5	2.0	1.9	2	1.5
N	6.6	4.7	2.7	2	0.1
S	0.1	0.2	0.4	0.1	0
Cl	0.3	0.1	0.01	0.02	0.7
HHV	16.3	24.5	26.3	26.3	26.9





# Biocoal compactation for sintering process



# BIOCOAL PREPARATION AND TESTING

1. > 50 kg biocoal powder dry mixing with starch (3-4% db)
2. Hot water added (> 70°C)
3. Pelletization performed in a 30 kg/h unit
4. Wet pellet dried in oven at 105°C overnight

## RESULTS

- ❖ Water resistant
- ❖ High durability
- ❖ No dust formation during storage



# Biocoal use as carburizer





# BIOCOAL CARBURIZATION TEST



Biocoal origin	Mass Fe (g)	Carburizing C (%)	C fix in biocoal (%)	C stoichiometric (g) to add	Biocoal to add (g)	Added biocoal (30% more)
OFMSW	150	3	63.4	4.5	7.10	10.14
Digestate	150	3	64.2	4.5	7.01	10.01
Straw	150	3	65	4.5	6.92	9.89
Sludge	150	3	42	4.5	10.71	15.31

# RESULTS OF CARBURIZATION TEST



Melting test N.	C (%)	S (%)	N (%)	O (%)	Added biocoal (g)	Pure Fe (g)	C in the hot metal (%)
1 (Biocoal OFMSW)	5.17	0.013	0.0046	0.011	17	150.25	69.2
2 (Digestate)	3.81	0.022	0.0059	0.0055	20.02	150.05	41.4
3 (Straw)	5.12	0.0085	0.0023	0.0068	20.15	150.45	55.4
4 (Sludge)	2.05	0.018	0.0021	0.0076	20	150.5	35.1

# Biocoal use as catalyst in catalytic methane pyrolysis





# H2STEEL in a Nutshell

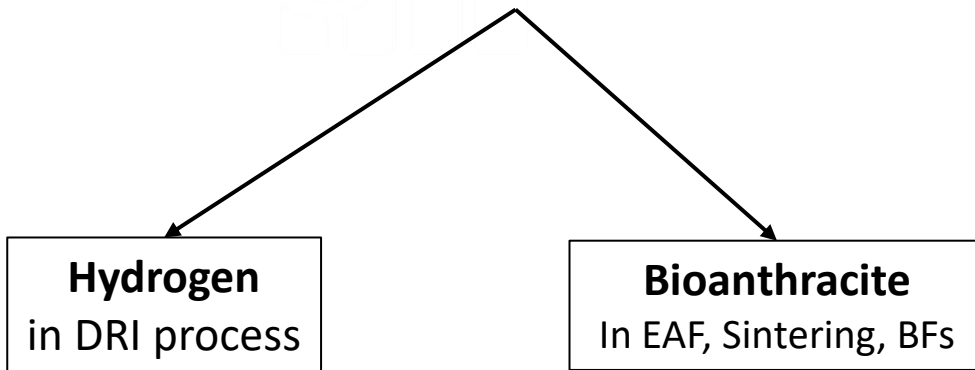
## Catalyst:

Biocoal obtained from sludge, digestate, and other biowaste

## Products:

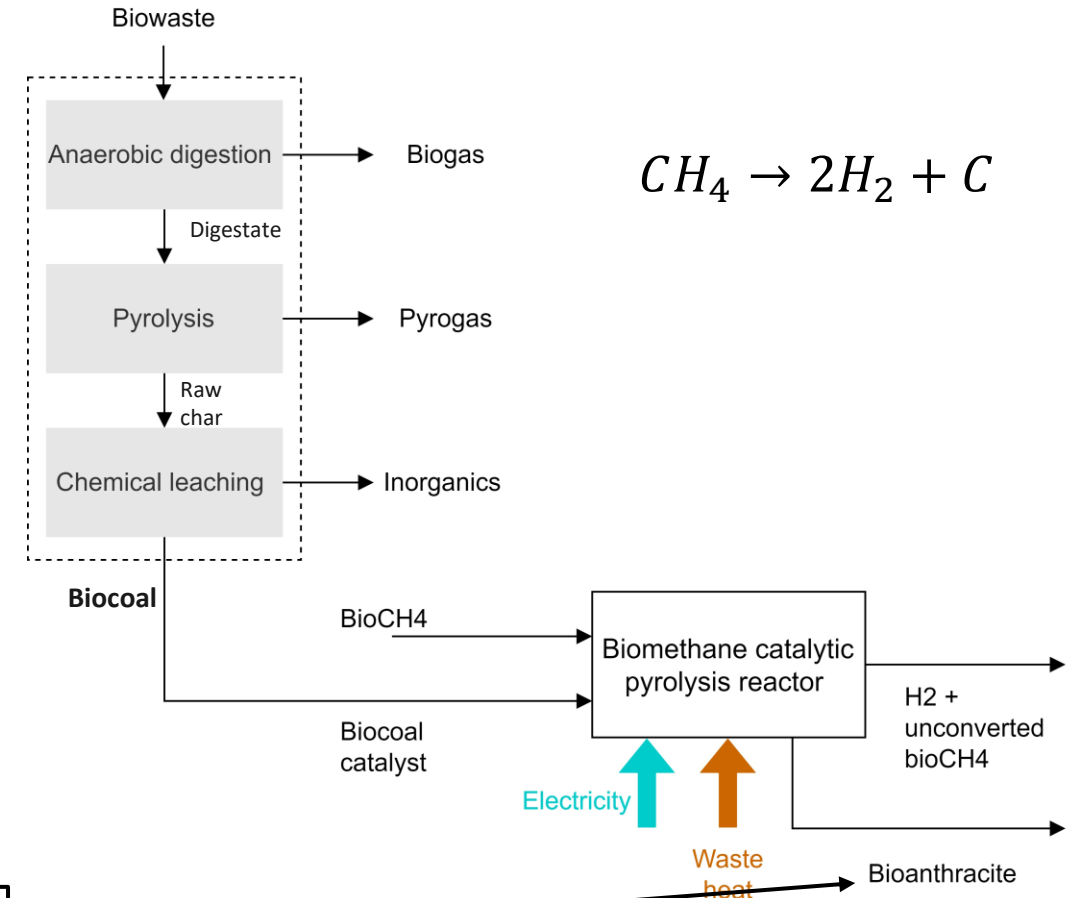
- Hydrogen
- Upgraded Bio-coal (C-enriched)

Targeted sector: Steel sector



After catalytic methane pyrolysis spent catalyst is a low volatile, C-enriched biocoal

## Conversion technology: catalytic methane pyrolysis process



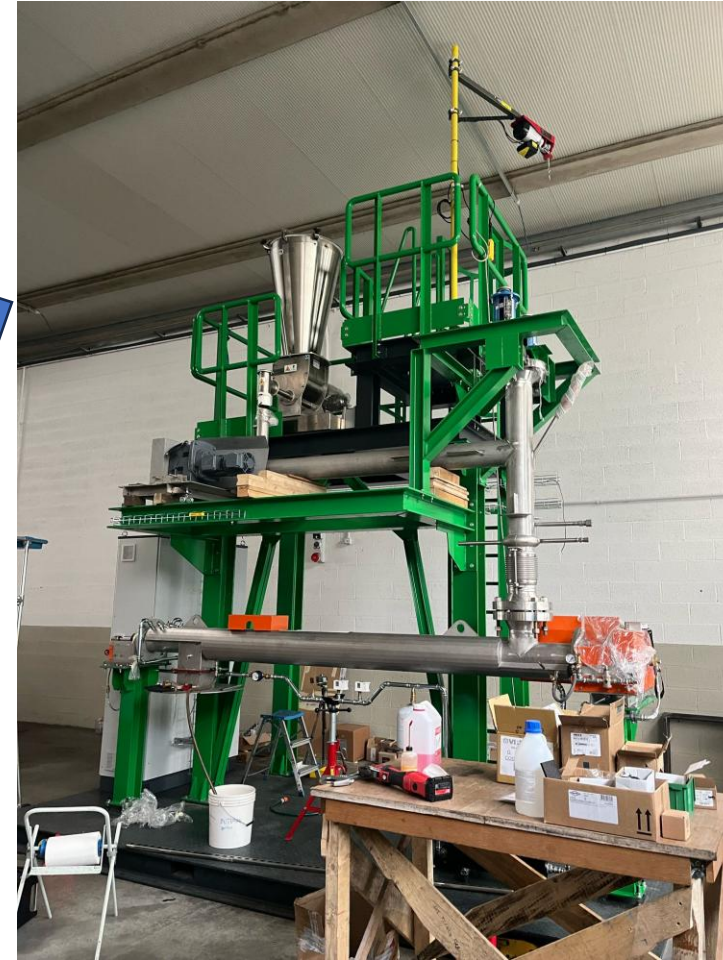
# H2STEEL: from lab tests to POC

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 **RE·CORD**



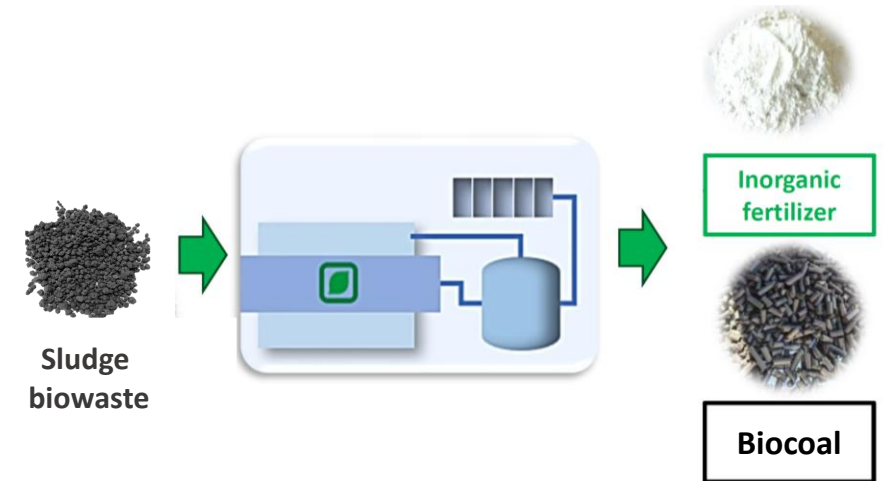
**HOMER**

**Continuous  
biocoal based  
catalytic  
methane  
pyrolysis unit**

# CONCLUSIONS

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- A 95-99% P extraction efficiency is obtained
- Sludge ash is extraction can be by up to 90%
- Biocoal has reduced reactivity at high Temperatures
- Silica is not removed by the process
- Calorific value is increased from 15-20 to 24-27 MJ/kg
- Leaching process remove PAH, Cl, and > 50% ash from char
- Nutrients recovery improve the economic feasibility and sustainability





# FOLLOW UP

3 tons char  
production  
in 100 kg/h  
rotary kiln



**PYROK rotary kiln**



> 1.3 tons  
biocoal  
production in  
a 500 lt/h  
leaching unit



**ADELE leaching unit**





# Thanks for the attention!



**Andrea Salimbeni, PhD**

Head of Unit | Raw materials & carbon recycling

[andrea.salimbeni@re-cord.org](mailto:andrea.salimbeni@re-cord.org)

[www.re-cord.org](http://www.re-cord.org)