

ESTEP Focus Groups
Smart Factory and
Circular Economy & Sustainability



# Digital-4-Environment ESTEP Workshop

Overview, recent developments and future trends

A Digital toolkit to investigate and guide the transition towards H<sub>2</sub>-DRI-based steelmaking considering the effects on energy management



- > Steelmaking Challenges
- ➤ MaxH<sub>2</sub>DR
- > Process chain multipurpose simulation toolkit
  - Gas and energy network models
  - Server interconnection Database
  - Models interactions
- **≻**Conclusions & Ongoing Work





# Steelmaking challenges

# Today



**EU** steel production accounts for 20-25 % industrial CO<sub>2</sub> emissions covered by the **Energy Taxation Directive (ETD)** 

### Morrow



2030

Developing technologies reducing CO<sub>2</sub> emissions from steel production by 50%

2050

Developing deployable technologies ultimately achieving climate neutrality





# Steelmaking challenges

Activities and projects are ongoing for guiding steel industry during its transition towards C-lean processes

Hydrogen based Direct reduction is considered one of the most attractive and ground-breaking C-lean solutions

Uncertainties and lack of experience with H2 content >80% exist related to:

technological aspects

effects on the global management of facilities from the point of view of production processes, energy production, demand and distribution





# MaxH<sub>2</sub>DR

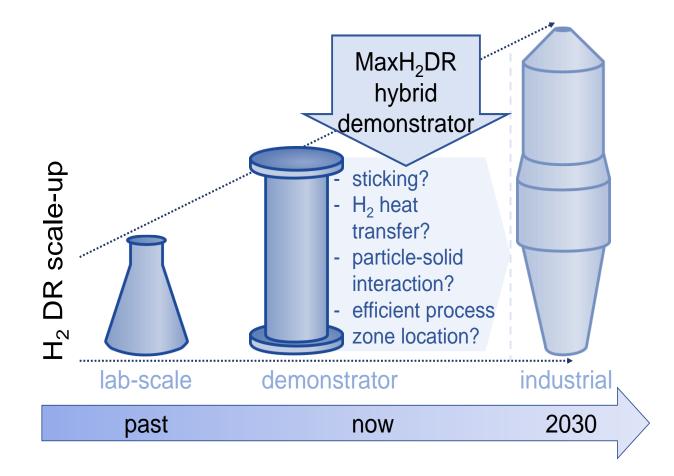


#### « from research to deployment of ground-breaking technologies for steel »



#### **Crucial aspects**

- Flow distribution
- Uniformity of gas and burden
- Spatial differences
- Process stability and efficiency issues



#### MaxH<sub>2</sub>DR will:

- close the current knowledge gaps hindering efficient scale-up
- deliver the tools needed for industrial implementation, process optimization, process integration and investment planning





# MaxH<sub>2</sub>DR

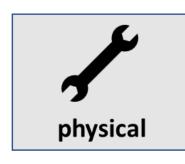


#### Approach: hybrid demonstration of steelmaking via H<sub>2</sub> based direct reduction

validating and fusing DR furnace models with physical demonstration into a "hybrid demonstrator"

#### **Hybrid Demonstration:**

#### Three perspectives of investigation:



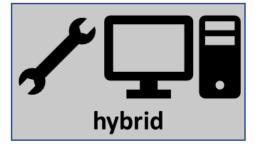
limited scale



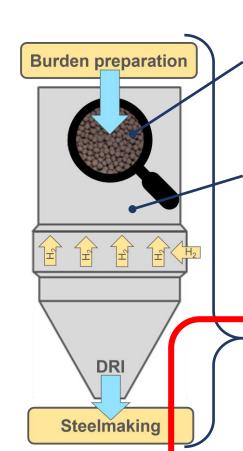


scale-up





large scale



"Particle scale"

- Laboratory experiments
- Kinetic sub-models

#### "DR shaft furnace scale"

- Bulk flow experiments (in demo plant)
- 3 detailed shaft furnace models
- Validation & process optimisation

### "Steelmaking process chain scale"

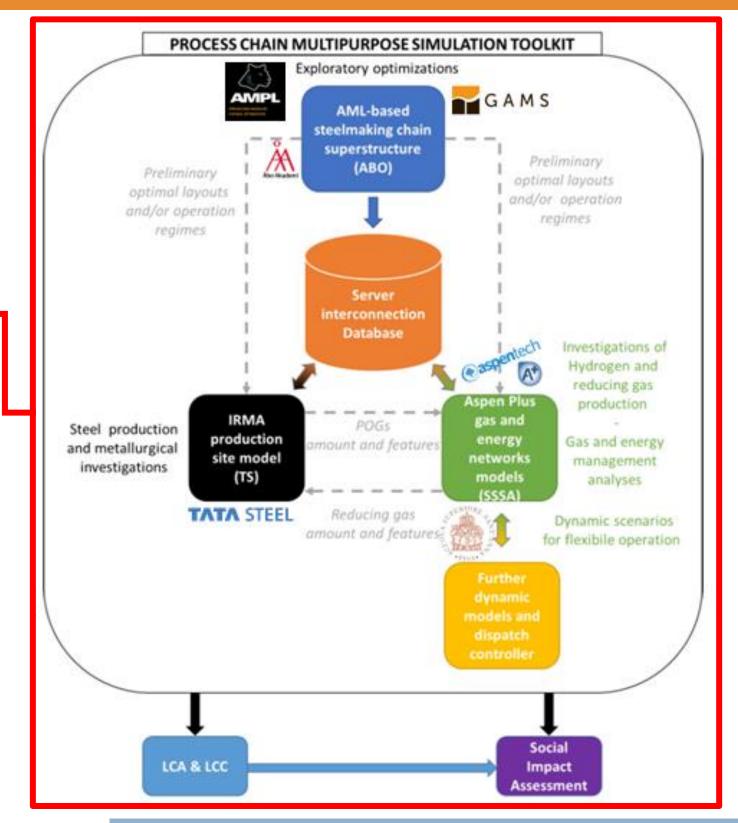
- Stationary scenario analyses
- Dynamic investigations (flexibility)
- LCA, LCC, social impacts





# Process chain multipurpose simulation toolkit

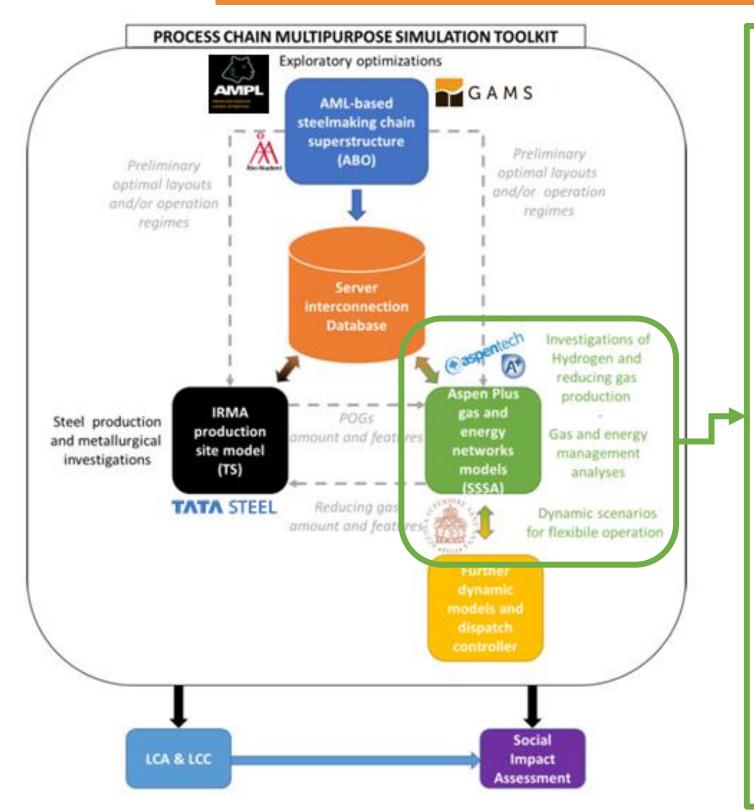
- Models for steelmaking process chain simulations allowing:
  - Scenario simulations with different site configurations
    - Starting route: standard integrated steelmaking
    - Intermediate route: mixed/hybrid configurations including CH<sub>4</sub>/H<sub>2</sub> based DRI process
    - Target route: H<sub>2</sub>-DRI-based steelmaking
  - Optimisation of DR process integration in integrated plants







### Gas and energy networks models

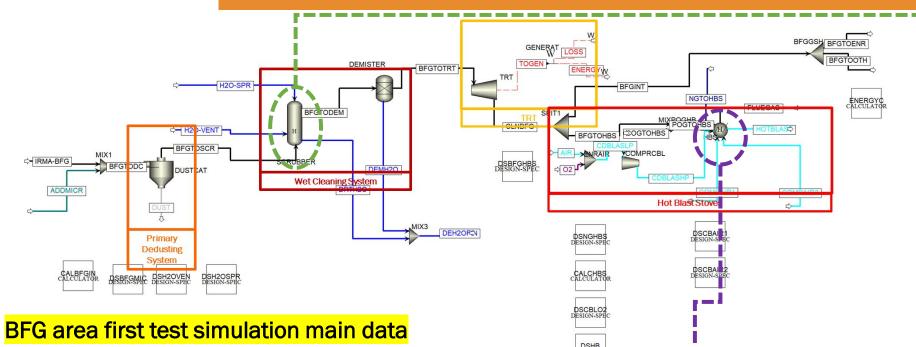


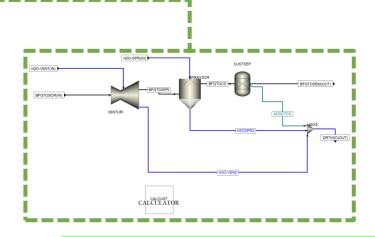
- Models for simulating energy streams management:
  - Gas cleaning and distribution \*
  - Steam production and distribution \*
  - Electricity production and distribution\*
  - \*Distribution based on demand from upstream simulation/process
- All the units models can receive and provide data from/to upstream models or directly from/to the plant through the "Server Interconnection Database"
- Now:
  - stationary models for all main units related to gas, steam and energy areas in standard integrated steelworks  $\rightarrow$  starting point and reference for the investigation of a gradual transition
- Future:
  - new stationary units to simulate the changes related to the DRI-based route and the use of hydrogen in the process
  - Dynamic models





# BFG area model

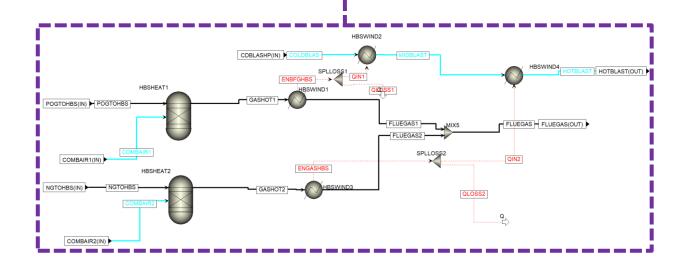




#### Main outputs of BFG area model

UoM	BFG1	BFG2				
Hot Blast						
t/h	189.29	289.30				
°C	1141	1141				
bara	4.4	4.4				
	70.76	70.76				
9/ mal	28.00	28.00				
/611101	0.04	0.04				
	1.20	1.20				
BFG	ì					
%	21.90	21.98				
kNm³/h	52.11	79.58				
t/h	71.46	109.16				
GJ/h	191.21	292.10				
%	73.02	72.95				
kNm³/h	173.73	264.14				
t/h	238.25	362.29				
GJ/h	637.48	969.51				
%	5.08	5.07				
kNm³/h	12.08	18.36				
t/h	16.56	25.19				
GJ/h	44.32	67.40				
Flue G	as					
kNm³/h	112.37	171.72				
t/h	157.31	240.41				
	24.41	24.42				
	0.18	0.18				
%mol	6.81	6.82				
	66.30	66.28				
	1.78	1.78				
na of /Ninc 3	1242.27	1243.61				
mg/mm <sub>2</sub>	1.52	1.52				
	Hot BI t/h ° C bara  %mol  BFG % kNm³/h t/h GJ/h % kNm³/h t/h GJ/h % kNm³/h t/h GJ/h % kNm³/h t/h GJ/h t/h	Hot Blast           t/h         189.29           °C         1141           bara         4.4           70.76         28.00           0.04         1.20           BFG           %         21.90           kNm³/h         52.11           t/h         71.46           GJ/h         191.21           %         73.02           kNm³/h         173.73           t/h         238.25           GJ/h         637.48           %         5.08           kNm³/h         12.08           t/h         16.56           GJ/h         44.32           Flue Gas           kNm³/h         112.37           t/h         157.31           24.41         0.18           %mol         6.81           66.30         1.78           mg/Nm³         1242.27				

Variable	UoM	BFG1	BFG2	
CO		23.87	23.87	
CO <sub>2</sub>		23.82	23.85	
H <sub>2</sub>	%mol	4.61	4.61	
H <sub>2</sub> O		4.30	4.31	
N <sub>2</sub>		43.40	43.34	
HCN		14	10	
HCI		14	10	
NH <sub>3</sub>	mg/Nm³	0.	.5	
SO <sub>2</sub>		5	5	
$NO_2$		0.	.5	
Flowrate	kNm³/h	246.67	378.48	
riowiate	t/h	339.25	509.93	
Temperature	°C	177.1	176	
Pressure	bara	2.8	2.8	
Dust mass	t/h	4.26	6.39	
Dust content	g/Nm³	17.27	16.88	
	Dust compo	sition		
Al <sub>2</sub> O <sub>3</sub>		1.27		
CaO		1.86		
С		52.	.81	
Fe <sub>2</sub> O <sub>3</sub>		15.	.14	
Fe0	%wt	24.63		
H <sub>2</sub> O	70W L	0.29		
MgO		0.59		
S		0.34		
SiO <sub>2</sub>		27		
Other		0.	.8	



Data are referred to a European integrated standardized steel mill (EU SSM) with 4 Mt<sub>HRC</sub>pa capacity

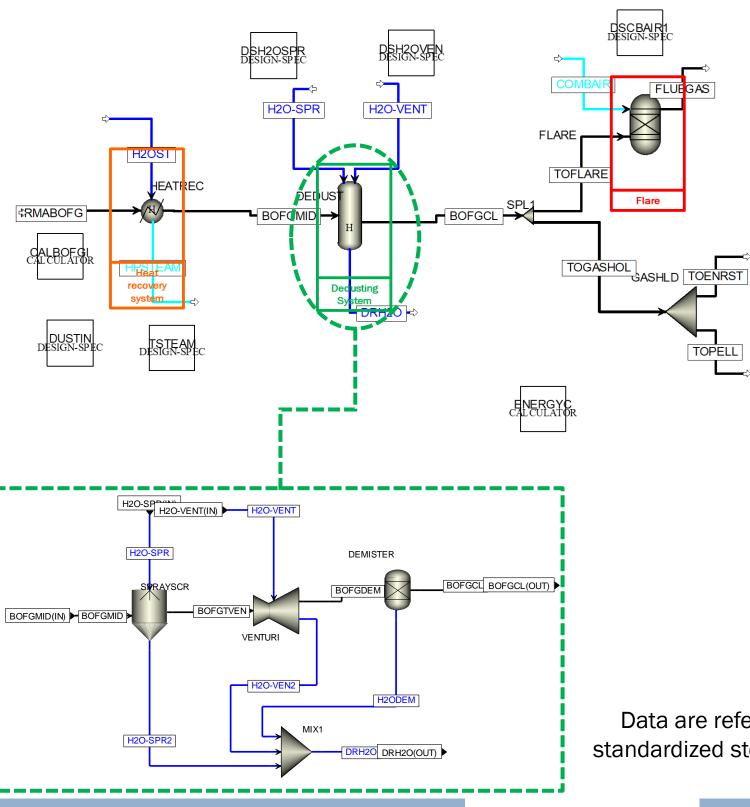




# BOFG area model

FLUEGAS

TOPELL



#### **BOFG** area first test simulation main data

Variable	UoM	BOFG
CO	John	64.18
CO <sub>2</sub>		14.27
H <sub>2</sub>	%mol	3.39
02		0.59
N <sub>2</sub>	%mol  kNm³/h t/h °C bara t/h	17.58
Doureto	kNm³/h	42.63
Flowrate	t/h	55.99
Temperature		1650
Pressure	bara	1
Dust mass		3197.25
Dust content	g/Nm³	75
Dust (	Compositio	on
Al <sub>2</sub> O <sub>3</sub>		3.8
CaO		1.1
Fe <sub>2</sub> O <sub>3</sub>		9.4
FeO	0/ vet	49.3
S	70 <b>W</b> L	0.13
SiO <sub>2</sub>		1.6
Fe		11.6
CaCO <sub>3</sub>		23.2
D	ust PSD	
0-0.5 μm		22
0.5-1 μm		16
1-3 µm	0/14	23
3-6 µm	70 <b>W</b> L	16
6-10 µm		12
10-15 μm		11

Data are referred to a European integrated standardized steel mill (EU SSM) with 4 Mt<sub>HRC</sub>pa capacity

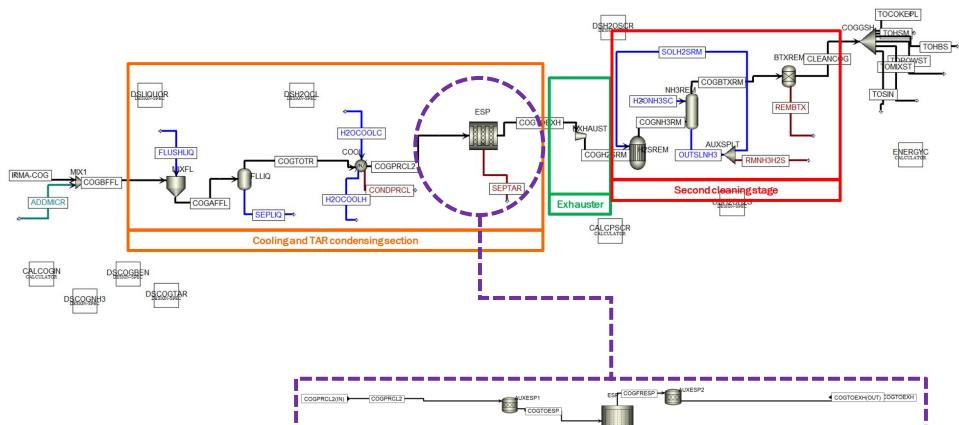
#### Main outputs of BOFG area model

variable	UOIVI	DUFG
Flowrate	kNm³/h	42.80
riowrate	t/h	56.12
CO		63.93
$CO_2$		14.21
H <sub>2</sub>	0/ m al	3.38
H <sub>2</sub> O	%mol	0.38
$N_2$		17.51
$O_2$		0.59
BOFG [	Distribution	n
	%	79.79
To M&ES	kNm³/h	34.15
TO MIGES	t/h	44.78
	GJ/h	287.84
	%	20.21
To Pellet Plant	kNm³/h	8.65
TO PENEL FIAME	t/h	11.34
	GJ/h	72.91



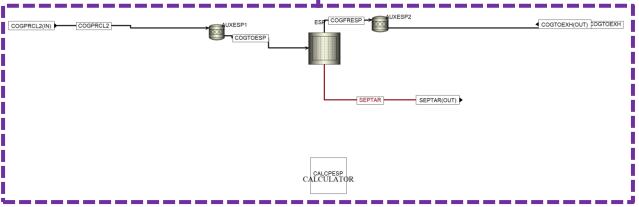


# COG area model



### COG area first test simulation main data

Variable	UoM	COG1	COG2	
C <sub>2</sub> H <sub>6</sub>		2.94		
CH <sub>4</sub>		26	.75	
CO	%mol	4.43		
CO <sub>2</sub>	7011101	0.04		
H <sub>2</sub>		65.34		
N <sub>2</sub>		18.55		
Flowrate	kNm³/h	21.66	33.16	
riowrate	t/h	7.60	11.64	
Temperature	°C	1100		
Pressure	bara	1		



Data are referred to a European integrated standardized steel mill (EU SSM) with 4 Mt<sub>HRC</sub>pa capacity

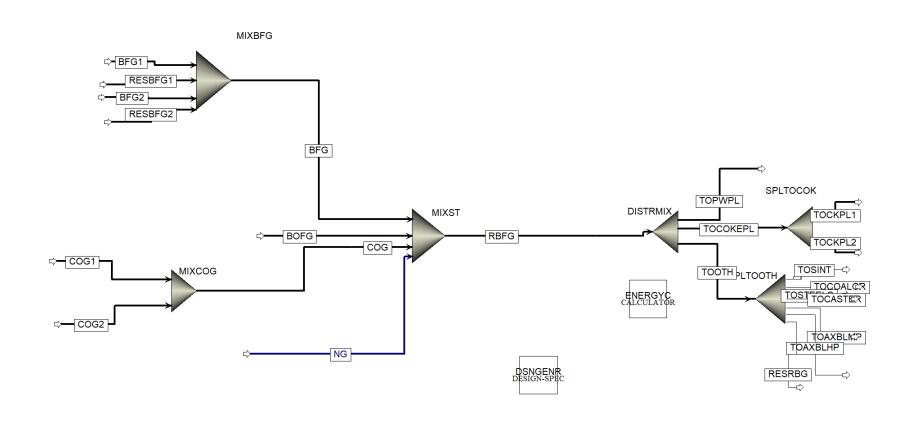
### Main outputs of COG area model

Variable	UoM	COG1	COG2	
Flowrate	kNm³/h	22.35	34.24	
riowiate	t/h	8.26	12.63	
C <sub>2</sub> H <sub>6</sub>		2.86	2.85	
CH₄		25.95	25.96	
CO		4.30	4.30	
CO <sub>2</sub>	%mol	0.04	0.04	
H <sub>2</sub>		63.39	63.38	
H <sub>2</sub> O		2.78	2.79	
$N_2$		0.18	0.18	
CO	G Distribut			
	%	2		
To Coke Plant	kNm³/h	5.59	8.56	
TO CONC I Idilic	t/h	2.06	3.16	
	GJ/h	105.36	161.30	
	%	51		
To Hot Rolling Mill	kNm³/h	11.40	17.46	
TO FIOL ROILING WIIII	t/h	4.21	6.44	
	GJ/h	214.94	329.05	
	%	18		
To HBS	kNm³/h	4.02	6.16	
101103	t/h	1.49	2.27	
	GJ/h	75.86	116.14	
	%	C		
To Power Station	kNm³/h	C	)	
10 I OWEI Station	t/h	C		
	GJ/h	C		
	%	3		
To M&ES	kNm³/h	0.67	1.03	
10 MQLS	t/h	0.25	0.38	
	GJ/h	12.64	19.36	
	%	3	3	
To Sinter Plant	kNm³/h	0.67	1.03	
TO SHITCH FIAIR	t/h	0.25	0.38	
	GJ/h	12.64	19.36	





# Mixing and Enrichment Station



#### Simulated rBFG distribution

User	UoM	rBFG
	%	65.00
	kNm³/h	327.70
Power Plant	t/h	446.99
	GJ/h	1324.55
	%	5.54
Cake Blant 1	kNm³/h	27.92
Coke Plant 1	t/h	38.08
	GJ/h	112.84
	%	8.39
Coke Plant 2	kNm³/h	42.31
CORE Plant 2	t/h	57.71
	GJ/h	171.00
	%	0.19
Cintan Diant	kNm³/h	0.94
Sinter Plant	t/h	1.28
	GJ/h	3.80
	%	1.38
Coal Grinding Line	kNm³/h	6.95
Coal Gilliang Line	t/h	9.47
	GJ/h	28.10
	%	2.83
Stoolehon	kNm³/h	14.25
Steelshop	t/h	19.44
	GJ/h	57.60
	%	0.30
Caster	kNm³/h	1.51
Caster	t/h	2.06
	GJ/h	6.10
	%	22.15
Auxiliary Boiler (MP steam)	kNm³/h	11.16
Auxiliary Boller (MP Steam)	t/h	15.23
	GJ/h	45.13
	%	0
Auxiliary Boiler (HP steam)	kNm³/h	0
Auxiliary boller (HP steam)	t/h	0
	GJ/h	0
	%	14.16
Residual rBFG	kNm³/h	71.41
Residual IDFG	t/h	97.41
	GJ/h	288.65

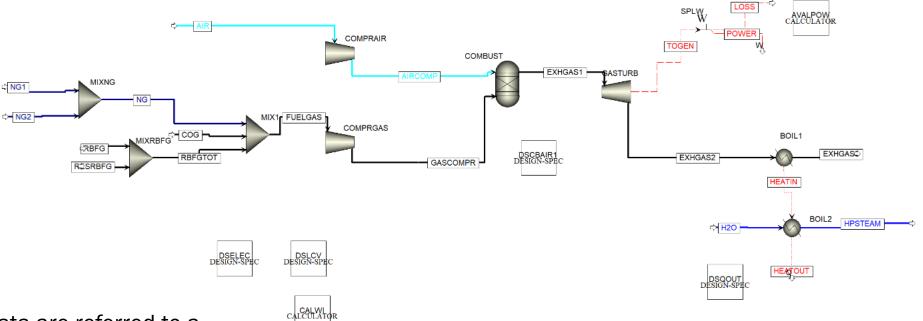
Data are referred to a European integrated standardized steel mill (EU SSM) with 4  $\rm Mt_{HRC}$ pa capacity





### Power Plant & Auxiliary boilers models

### Power Plant model

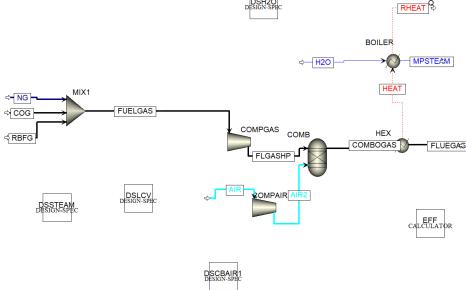


### Main inputs and outputs of Power plant model

Variable	UoM	Value
	kNm³/h	399.11
rBFG	t/h	544.18
NG	kNm³/h	1.14
ING	t/h	0.88
Fuel Gas WI	MJ/Nm <sup>3</sup>	4.38
Produced electric power	MW	129.82
Produced HP steam	t/h	351.74

Data are referred to a European integrated standardized steel mill (EU SSM) with 4 Mt<sub>HRC</sub>pa capacity

### Auxiliary boilers model

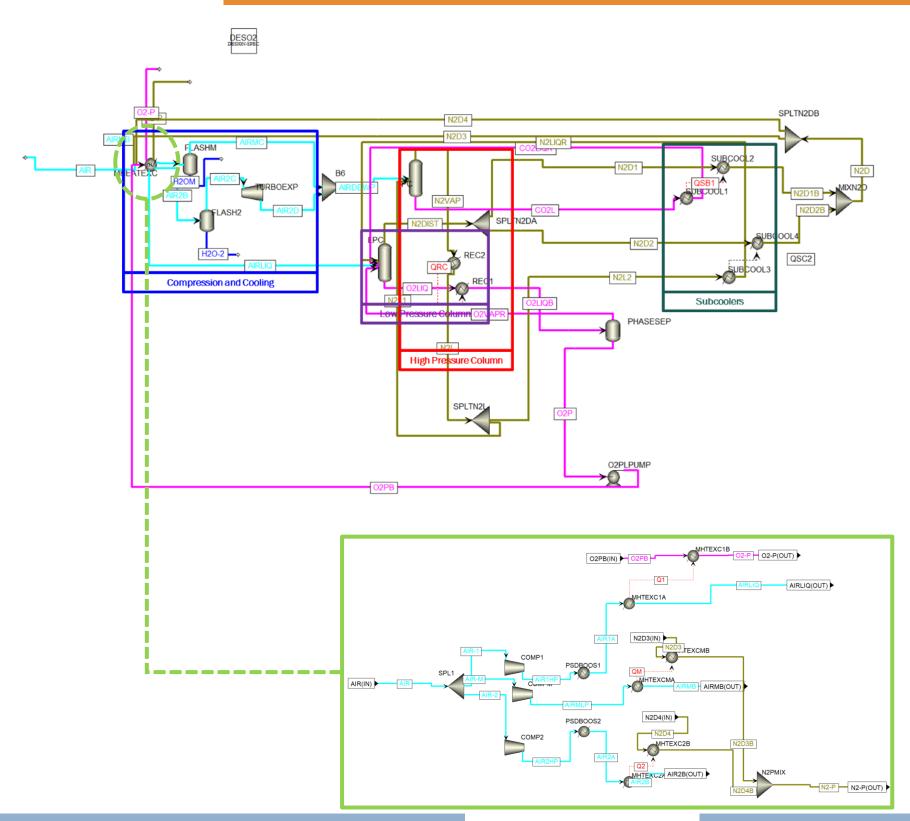


MP steam of 15.3 t/h is produced by using an amount of 11.16 kNm<sup>3</sup>/h (152.15 t/h) of rBFG.





# ASU model



#### Main outputs of ASU model

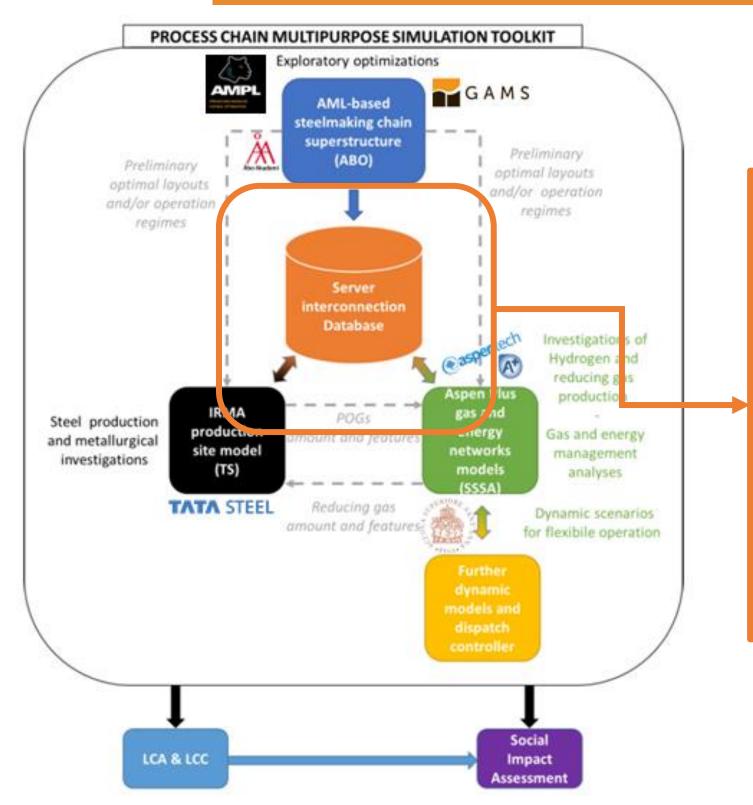
Variable	UoM	Value
	kNm³/h	57.34
$O_2$	t/h	81.15
	%mol (purity)	95.64
	kNm³/h	210.26
N <sub>2</sub>	t/h	262.95
	%mol (purity)	99.57

Data are referred to a European integrated standardized steel mill (EU SSM) with 4 Mt<sub>HRC</sub>pa capacity





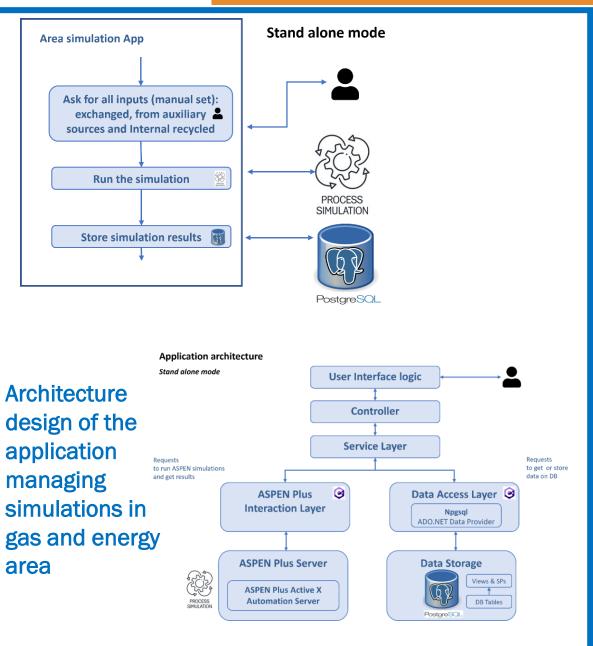
### Server interconnection Database

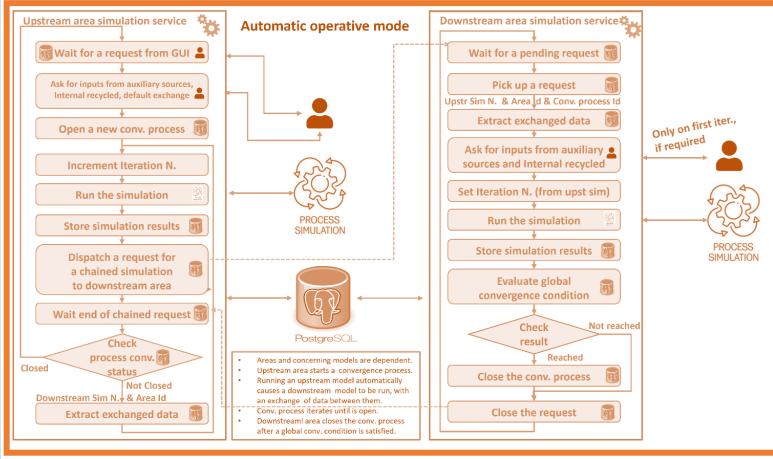


- Complex IT architecture for allowing the connection of the energy network models to upstream process models or directly to plant/pilots:
  - Receiving data
  - Using data
  - Making automatic investigations
- It includes:
  - Dedicated PostgreSQL relational database
  - Stored procedures
  - Further methods



# Server interconnection Database





#### Two modes of operation of the system are envisaged:

- **stand-alone mode** → each model is considered as independent
  - Possibility to use user settled data or real industrial data
- automatic mode  $\rightarrow$  the different area models are dependent and connected within a global process





# Models interaction

Correct interaction between process models and gas and energy network models have been demonstrated through the right satisfaction of balances and heat and energy demands

User	Heat Demand by gas	Gas distribution				
user	GJ/h	BFG	rBFG	BOFG	COG	NG
	43/11			GJ/h (t/h)		
Coke Plant 1	218.20		112.84 (38.08)		105.36 (2.06)	
Coke Plant 2	332.30		171.00 (57.71)		161.30 (3.16)	
Sinter Plant	35.80		3.80 (1.28)		32 (0.63)	
Pellet Plant	72.90			72.91 (11.34)		
Coal Grinding Line	28.10		28.10 (9.47)			
Blast Furnace 1 (for HBS)	267.07	191.21 (71.46)			75.86 (1.49)	
Blast Furnace 2 (for HBS)	408.24	292.10 (109.16)			116.14 (2.27)	
Steelmaking Shop	57.60		57.60 (19.44)			
Casters	6.10		6.10 (2.06)			
Hot Rolling Mill	630.10				543.99 (10.65)	86.11 (1.86)
Power Plant	1653.94		1613.2 (544.4)			40.74 (0.88)
Auxiliary Boilers (MP+HP)	45.13		45.13 (15.23)			





# Models interaction

Correct interaction between process models and gas and energy network models have been demonstrated through the right satisfaction of balances and heat and energy demands

	Electricity Demand	Total Electricity Demand	Electr	ricity distrib	ution
User	G.	J/h	Power Plant	TRT	External Grid
				GJ/h (%)	
Coke Plant 1 + exhauster	10.70+0.83				
Coke Plant 2 + exhauster	16.30 + 1.27				
Sinter Plant	59.20				
Pellet Plant	19.90				
Coal Grinding Line	10.80				
Blast Furnace 1 (cold blast compressor)	33.42	542.51	467.34	28.08	45.98
Blast Furnace 2 (cold blast compressor)	51.07		(86.14)	(5.17)	(8.69)
Steelmaking Shop	63.90				
Casters	21.10				
Hot Rolling Mill	141.41				
Auxiliary Boilers (MP+HP)	0.73				
ASU	111.880				

		team emand	Total Stea Demand		Steam Distribution	
User					HP	MP
	HP	MP	HP	MP	BOFG Area + Power Plant +	Auxiliary
					Auxiliary Boilers	Boiler
			t/h		t/h (t/h of residual steam	)
Coke Plant 1	4.2	0				
Coke Plant 2	6.5	0				
Sinter Plant	0	0.7				
Pellet Plant	0	0.2				
Coal						
Grinding	0	0				
Line						
Blast	0	1.0	10.7	15.3	10.7 (361.07)	15.3
Furnace 1	Ů	1.0	10.7	10.0	10.7 (301.07)	10.0
Blast	0	1.6				
Furnace 2	Ů	1.0				
Steelmaking	0	8.6				
Shop	Ŭ					
Casters	0	0.5				
Hot Rolling Mill	0	2.7				

User	Demand		Total Demand		Distribution	
	O <sub>2</sub>	N <sub>2</sub>	O <sub>2</sub>	N <sub>2</sub>	O <sub>2</sub> (from ASU)	N <sub>2</sub> (from ASU)
	t/h				t/h (t/h of residual)	
Coal Grinding Line		3.40				
Blast Furnace 1 (for cold blast O <sub>2</sub> enrichment)	20.39					2.00
Blast Furnace 2 (for cold blast O <sub>2</sub> enrichment)	31.16				81.15 (0)	3.80 (259.15)
Steelmaking Shop	29.60	0.20				
Hot Rolling Mill		0.20				





# Conclusions & Ongoing Work

The transition towards H<sub>2</sub>-DRI-based steelmaking requires closing the current knowledge gaps existing from the particle to the process chain scales

Concerning process chain scale, modifications in process route can be translated in significant changes in energy streams managements

During MaxH<sub>2</sub>DR EU project, among the other activities of providing a hybrid demonstrator, a process chain digital toolkit including models for simulating gas, steam and all the energy streams management area is under development

Models of units related to the management of gas, steam and energy streams in standard steelworks have been developed, showed and its interaction with process model demonstrated as starting point and reference for transitions simulations

A complex IT asrchitecture has been developed for using the gas and energy network models linked to process chain models or by using directly plant data and allowing stand-alone or automatic modes

Other models are under developments for considering new units for allowing the simulations of transition steps starting from standard integrated route, passing from mixed/hybrid route (BF/BOF+CH<sub>4</sub>/H<sub>2</sub>-DRI/EAF) and achieving full H<sub>2</sub>-DRI steelmaking





